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AIR MEASUREMENT SERVICES.

Horizon Test #: W07-035-FRA

Date Tested: April 23, 2003 Report Date: May 7, 2003

Revision Number: 0

ANNUAL EMISSIONS TEST OF LANDFILL GAS FLARE #1 BRADLEY LANDFILL

Permit to Construct No. 370136

Prepared for:

Waste Management Recycling and Disposal Services of California, Inc. 9081 Tujunga Avenue, 2nd Floor Sun Valley, California 91352

Prepared by:

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Regulatory Agency:

South Coast Air Quality Management District 21865 East Copley Drive Diamond Bar, California 91765

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May 7, 2003

Mr. Bruce Matlock Bradley Landfill and Recycling Center 9227 Tujuna Avenue Sun Valley, California 91352

Dear Mr. Matlock:

Please find enclosed three copies of the final report entitled "Annual Emissions Test of Landfill Gas Flare #1".

If you have any questions please call me at (805) 498-8781.

Sincerely,

HORIZON AIR MEASUREMENT SERVICES, INC.

Scott H. Bunch

Project Manager

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1. INTRODUCTION

Under the Bradley Landfill and Recycling Center (BLRC) site specific Rule 1150.1 compliance plan, Waste Management Recycling and Disposal Services of California, Inc. is required to conduct an annual source test on landfill gas Flare #1 located at BLRC (Permit to Construct #370136). Horizon Air Measurement Services, Inc. (Horizon) had been retained for this purpose.

All testing/analytical procedures conformed to those outlined in Horizon Test Plan No. W07-013-TP, which had been previously approved by the South Coast Air Quality Management District (SCAQMD). Horizon completed the source testing on April 23, 2003.

Two samples were taken for each parameter of interest (Table 1-1) with the exception of trace organic compounds and reduced sulfur compounds, for which only one sample per location was collected. The results of the testing program, with respect to Permit limits, are provided in Section 2 - Results Summary.

A brief description of the flare and flare operating conditions during testing is provided in Section 3. Section 4 provides a summary of sampling/analytical procedures utilized. Section 5 provides a more detailed results summary/discussion.

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Table 1-1
Compounds of Interest - Flare #1
Waste Management - Bradley Landfill
April 23, 2003

Parameter	Location	Method	Number of Samples Per Source
Total Non Methane Hydrocarbons	Inlet	SCAQMD Method 25.1	2
	Outlet	SCAQMD Method 25.3	2
Reduced Sulfur Compounds (C ₁ -C ₃) Including H ₂ S	Inlet	SCAQMD Method 307.91 Equivalent	1
Speciated Organic Compounds	Inlet	Whole Air/GC-MS (1150 list)	1
	Outlet	Whole Air/GC-MS (1150 list)	1
Particulate Matter	Outlet	SCAQMD Method 5.1	2
Oxides of Nitrogen	Outlet	SCAQMD Method 100.1	2
Carbon Monoxide	Inlet	SCAQMD Method 25.1	2
	Outlet	SCAQMD Method 100.1	2
Oxygen	Inlet	SCAQMD Method 25.1	2
	Outlet	SCAQMD Method 100.1	2
Carbon Dioxide	Inlet	SCAQMD Method 25.1	2
	Outlet	SCAQMD Method 100.1	2
Methane	Inlet	SCAQMD Method 25.1	2
	Outlet	SCAQMD Method 25,3	2
Flow Rate/Temperature	Inlet	SCAQMD Method 2.3	2
	Outlet	SCAQMD Method5.1/Calculated	2
Moisture	Outlet	SCAQMD Method 5.1	2
	Inlet	SCAQMD Method 4.1	2
BTU Content	Inlet	SCAQMD Method 25.1	2

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2. SUMMARY OF RESULTS

The results of the testing program conducted on Flare #1 are provided in Table 2-1. Emission rates of oxides of nitrogen, carbon monoxide, total particulate matter, total non-methane organics and total sulfur compounds (as SO₂) were within PTC 370136 (see Appendix H) limitations.

A more detailed discussion of results is provided in Section 5.

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Table 2-1 Summary of Results Flare #1 Waste Management - Bradley Landfill April 23, 2003

Parameter	Measured Emission Rate*	Permitted Emission Rate	
Inlet Gas Flow Rate	3531 dscfm	5556 cfm	
Oxides of Nitrogen, as NO ₂	2.48 lb/hr 0.030 lb/MMBtu	10.0 lb/hr, 0.06 lb/MMBtu	
Total Particulate Matter	0.53 lb/hr	3.0 lb/hr	
Carbon Monoxide	<3.75 lb/hr	33.3 lb/hr	
Total Non Methane Organics, as CH ₄	0.295 lb/hr	1.86 lb/hr	
Total Non Methane Organics, as C ₆	1.20 ppm C ₆ @ 3% O ₂	20 ppm C ₆ @ 3% O ₂ (Rule 1150.1)	
Total Sulfur Compounds, as SO ₂	2.25 lb/hr	8.44 lb/hr	

^{*} Measured emission rates shown are the average of two test runs (samples).

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3. FLARE DESCRIPTION AND OPERATION

3.1 Flare Description

The landfill gas flare is a John Zink enclosed flare consisting of an insulated steel cylinder 60 feet high and 156 inches outside diameter. The flare is equipped with a multi-jet burner, a propane gas pilot, electric igniter, UV flame sensor, thermocouple with temperature indicator and recorder, automatic shutdown and alarm system, automatic combustion air regulating system, temperature controller and flare arrestor. Landfill gas is supplied by a 200 horsepower (Hp) blower (one blower is standby). Operating landfill gas flow rate is limited, by the Permit, to 5556 cubic feet per minute. Landfill gas flow rate was continuously monitored using an annubar and is recorded digitally by the facility. Flare temperature and condensate injection rate was also continuously monitored by the facility.

Condensate flow rate is limited to five gallons per minute by the Permit.

3.2 Sample Location

Flare exhaust samples were obtained from each of two ports positioned at right angles, located five feet (0.4 diameters) from the top of the flare (144 inches inside diameter) and approximately 55 feet (4.6 diameters) above ground level.

Inlet samples and measured flow rate were obtained from the 14-inch diameter (13.25 inch inside diameter) landfill gas line supplying the flare at a location 144 inches (10.9 diameters) downstream and 93 inches (7.0 diameters) upstream of any flow disturbance.

3.3 Flare Operation During Testing

The following operating condition set points were maintained during the emissions testing:

Flare Temperature Set Point -

1650 °F

Landfill Gas Flow Rate -

3600 scfm

Condensate Injection Rate -

3.5 gpm

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The condensate injection operated in the normal automatic mode.	Flare process data is provided in
Appendix G.	

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4. SAMPLING/ANALYSES

The sampling/analytical program had been designed to quantify the parameters of interest outlined in Table 1-1.

4.1 Sample Location

4.1.1 Flare Exhaust

At the flare exhaust 24 sample points (12 per diameter), determined in accordance with Method 1.1, were utilized for the determination of the following compounds:

- · particulate matter
- NO_X
- CO
- O₂/CO₂
- · flow rate
- · moisture

The exact locations of the sampling points are provided in Appendix D, Field Data Sheets.

A description of SCAQMD Method 1.1 is provided in Appendix A.

One sample point near the center of the stack was utilized for the collection of the following compounds:

- speciated organic compounds
- · total non methane hydrocarbons
- · methane

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4.1.2 Landfill Gas Supply Line

Twelve sample points (six per diameter), determined in accordance with Method 1.1, were used for collection of the following parameter:

flow rate

The exact locations of the sampling points are provided in Appendix D, Field Data Sheets. A description of SCAQMD Method 1.1 is provided in Appendix A.

A single sample point was utilized for the collection of the following compounds:

- · total non methane hydrocarbons
- methane
- CO
- CO₂/O₂
- · reduced sulfur compounds
- speciated organic compounds
- BTU content
- · moisture

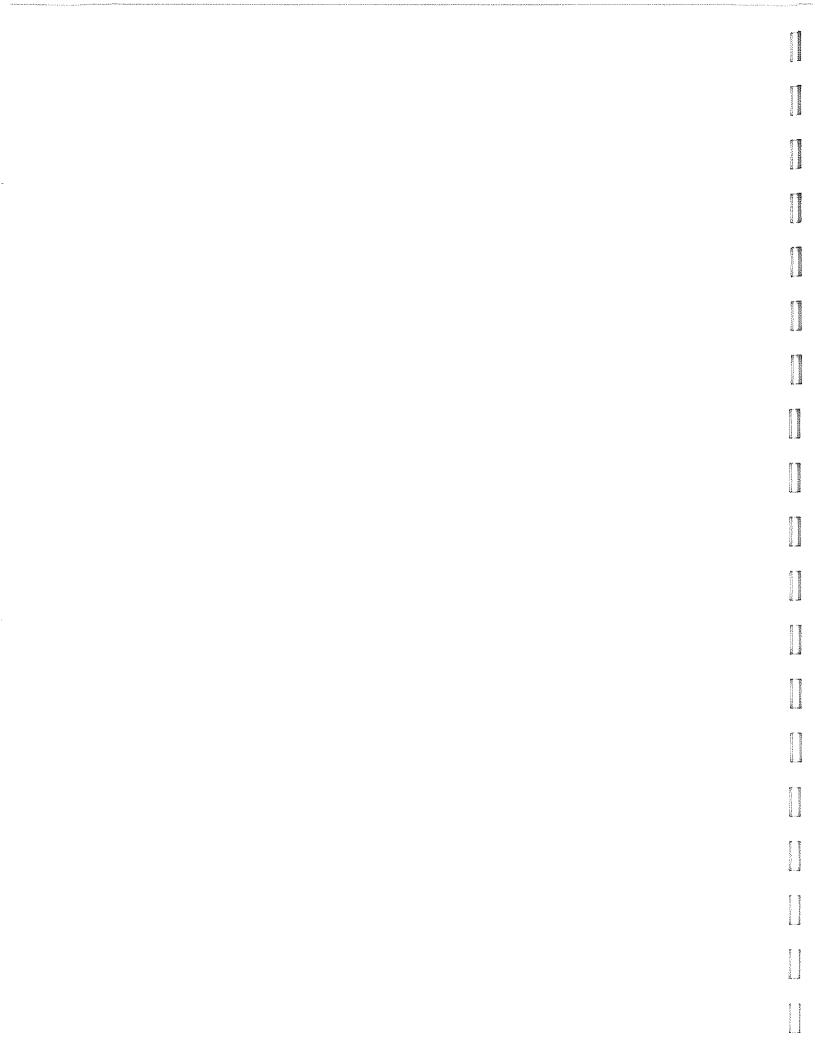
4.2 Moisture

4.2.1 <u>Inlet - SCAOMD Method 4.1</u>

Landfill gas moisture content was determined using SCAQMD Method 4.1. Two, one hour test runs were conducted in conjunction with the outlet particulate and SCAQMD Method 100 testing. A description of SCAQMD Method 4.1 is provided in Appendix A.

4.2.2 Outlet - SCAOMD Method 5.1

Moisture content of the flare exhaust was determined using SCAQMD Method 4.1 in conjunction with SCAQMD Method 5.1, as detailed in Appendix A.



4.3 Flow Rate

4.3.1 <u>Inlet - SCAOMD Method 2.3</u>

Landfill gas flow rate was determined using SCAQMD Method 2.3. A description of SCAQMD Method 2.3 is provided in Appendix A.

4.3.2 Outlet - SCAOMD Method 5.1

The landfill flare flow rate was monitored in conjunction with SCAQMD Method 5.1, as detailed in Appendix A. However, since the flare exhaust velocity was below the applicable limit (0.05 in. WG ΔP) of SCAQMD Method 2.1/5.1, the exhaust flow rate was calculated stoichiometrically based upon the landfill gas composition and stack dilution.

4.4 Particulate Matter (Outlet) - SCAQMD Method 5.1

Horizon conducted two, 60-minute test runs on the flare exhaust for particulate matter determination in accordance with SCAQMD Method 5.1 protocol. Twenty-four traverse points were utilized for the collection of particulate matter at the flare exhaust. A description of SCAQMD Method 5.1 is provided in Appendix A. Stack gases were withdrawn through an integral quartz nozzle and probe.

4.5 Oxides of Nitrogen, Carbon Monoxide, Carbon Dioxide, Oxygen (Continuous Emissions Monitoring) - SCAOMD Method 100.1

Two, 60-minute test runs were conducted at the flare exhaust. Twenty-four sample points were utilized. All sampling was performed under the guidelines of SCAQMD Method 100.1 as detailed in Appendix A.

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4.6 <u>Hydrogen Sulfide (H₂S), and C₁ - C₃ Sulfur Compounds (Inlet) - SCAQMD Method 307.91</u> Equivalent

Hydrogen sulfide and C_1 - C_3 sulfur compound samples were collected at the inlet of the flare using the Tedlar bag collection system depicted in Appendix A. All system components coming in contact with the landfill gas were Teflon.

Hydrogen sulfide and C_1 - C_3 sulfur compounds were analyzed using a Method 307.91 equivalent by AtmAA, Inc. Equivalency had been formally granted by SCAQMD to AtmAA, Inc. for this Method.

4.7 Speciated Organic Compounds - SCAQMD Rule 1150.1 List

4.7.1 Inlet

Speciated organic compounds were collected at the flare inlet of the landfill gas using the Tedlar bag collection system depicted in Appendix A. All system components coming in contact with the landfill gas were Teflon or stainless steel. Speciated organic compounds (SCAQMD Rule 1150.1 list) were identified and quantified using GC/MS analytical procedures.

4.7.2 Outlet

Speciated organic compound samples were collected in conjunction with the particulate/CEM testing at the outlet using the Tedlar bag method depicted in Appendix A. Each sample was then analyzed for speciated organic compounds (SCAQMD Rule 1150.1 list) using GC/MS procedures.

Management of the last Passagaranga (No. la constant in the second 4.8 Total Non Methane Hydrocarbons, Methane, Carbon Dioxide and Carbon Monoxide

4.8.1 Inlet - SCAQMD Method 25.1

Total non methane hydrocarbons, methane, CO₂ and CO concentration were determined at the flare inlet from duplicate samples using SCAQMD Method 25.1. A description of SCAQMD Method 25.1 is provided in Appendix A.

4.8.2 Outlet - SCAOMD Method 25.3

Duplicate samples were obtained for total non methane hydrocarbon and methane concentration determination using SCAQMD Method 25.3. A description of SCAQMD Method 25.3 is provided in Appendix A.

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5. RESULTS DISCUSSION

Detailed results of the criteria testing conducted on Flare #1 on April 23, 2003 are presented in Table 5-1. Speciated organic compound destruction efficiencies and emission rates are provided in Table 5-2. Since the flare exhaust velocity was below the applicable range (>0.05 ΔP inches water gauge) of SCAQMD Method 2.1, the flare exhaust flow rate for each test run was calculated stoichiometrically based upon the composition of the landfill gas and the exhaust stack dilution. Oxide of sulfur emission rate was calculated based upon the landfill gas total sulfur compound concentration and flow rate (see Appendix B).

Test Critique

No sampling or analytical problems or Method deviations were encountered during any phase of the test program.

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Table 5-1 Summary of Results Waste Management - Bradley Landfill Flare #1 April 23, 2003

· · · · · · · · · · · · · · · · · · ·	LA	NDFILL		FLARE EXHAUST						
Run Number	1	2	Avg.		1		2		Avg.	
STACK GAS CHARACTERIS	TICS									
Temperature, degrees F	141	143	142		1526		1523		1524	
Moisture, %	5.3	6.6	6.0		9.2		9.6		9.4	
Flow Rate, acfm	4334	4367	4350							
Flow Rate, dscfm	3549	3514	3531		41134	*	43527	*	42330	¥
Fixed Gases										
Oxygen, %	2.82	_	2.82		13.78		14.24		14.01	
Carbon Dioxide, %	33,50	-	33.50		6.46		6.08		6.27	
Methane, %	39.05	-	39.05		0.00		0.00		0.00	
BTU Value, Btu/scf	394	-	394		-		-			
EMISSIONS										
Oxides of Nitrogen										
ppm	-	-	-		8.5		7.7		8.1	
ppm @ 3 % O2	-	-	-		21.3		20.6		20.9	
lb/hr	-	-	-		2.532		2.427		2.479	
lb/MMBtu	-	-	-		0.030		0.029		0.030	
Carbon Monoxide										
ppm	_	-	-	<	20.0	<	20.0	<	20.0	
ppm @ 3 % O2	_	-	-	<	50.3	<	53.7	<	52.0	
lb/hr	_	-	-	<	3.64	<	3.85	<	3.75	
lb/MMBtu	-	-	-	<	0.04	<	0.05	<	0.04	
Total Particulate Matter										
gr/dscf	-	-	-		0.0015		0.0014		0.0015	
lb/hr	-	-	-		0.51		0.54		0.53	
Total Non-Methane Hydrocarbons	3									
(Reactive Organic Compounds)										
ppm, as Methane	10187	-	10187		2.76		-		2.76	
lb/hr, as Methane	90.93	-	90.93		0.295		-		0.295	
Sulfur Compounds										
Hydrogen Sulfide, ppm	48.4	_	48.4		0.50		-		0.50	
Total Sulfur, ppm as H2S	62.8	_	62.8		-		-		-	
Oxides of Sulfur**										
lb/hr	_	_	_		2.25		_		2.25	

^{*} Flow Rate calculated stoichiometrically

^{**} Calculated from sulfur balance

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Table 5-2
Trace Organic Species
Destruction Efficiency Results
Waste Management - Bradley Landfill
Flare #1
April 23, 2003

	Inlet				Outlet					
Species	C	Concentration (ppb)		Emission Rate (lb/hr)	Concentration (ppb)		Emission Rate (lb/hr)	Destruction Efficiency (%)		
Hydrogen Sulfide		48400		9.21E-01	<	500	<	1.14E-01	>	87.62
Benzene		2890		1.26E-01	<	0.3	<	1.57E-04		99.88
Benzychloride	<	40	<	2.84E-03	<	0.8	<	6.80E-04	>	NA
Chlorobenzene		211		1.33E-02	<	0.3	<	2.27E-04	>	98.30
Dichlorobenzenes		1480		1.21E-01	<	1.1	<	1.08E-03	>	99.11
1,1-diehloroethane		796		4.40E-02	<	0.3	<	1.99E-04	>	99.55
1.2-dichloroethane		134		7.41E-03	<	0.3	<	1.99E-04	>	97.32
1.1-dichloroethylene		162		8.77E-03	<	0.3	<	1.95E-04	>	97.78
Dichloromethane		5300		2.52E-01	<	0.3	<	1.71E-04	>	99.93
1.2-dibromoethane	<	16	<	1.68E-03	<	0.3	<	3.77E-04		NA
Perchloroethene		3320		4.39E-01	<	0.2	<	3.17E-04	>	99.93
Carbon tetrachloride	<	20	<	1.72E-03	<	0.2	<	2.06E-04	>	NA
Toluene		66200		3.40E+00	<	0.8	<	4.93E-04	>	99.99
1.1.1-trichloroethane		59		4.40E-03	<	0.2	<	1.78E-04	>	95.95
Trichloroethene		1380		1.01E-01	<	0.2	<	1.75E-04	>	99.83
Chloroform	<	16	<	1.06E-03	<	0.2	<	1.59E-04	>	NA
Vinyl Chloride		454		1.58E-02	<	0.3	<	1.25E-04	>	99.21
m xylenes		29800		1.76E+00	<	0.5	<	3.55E-04	>	99.98
o- p xylene		7730		4.57E-01	<	0.3	<	2.13E-04	>	99.95
TNMHC		10187217	7	9.10E+01		2755		2.95E-01		99.68

Note: All values preceded by "<" are below the detection limit - reported values are detection limit values. NA-Not applicable: Destruction efficiency cannot be calculated since both inlet and outlet values are helow the detection limit.

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APPENDIX A - Sampling and Analytical Methods

Method:

Sample Velocity Traverses for Stationary Sources

Applicable for Methods:

EPA Method 1, SCAQMD Method 1.1, CARB Method 1

Principle:

To aid in the representative measurements of pollutant emissions and/or total volumetric flow rate from a stationary source, a measurement site where the effluent stream is flowing in a known direction is selected, and the cross section of the stack is divided into a number of equal areas. A traverse point is then located within these equal areas. The method cannot be used when, 1) flow is cyclonic or swirling, 2) stack is small than about 0.30 meter (12 inches) in diameter or 3) the measurement of the site is less than two stack or duct diameters downstream or less than a half diameter upstream from the flow disturbance.

Stack Gas Velocity and Volumetric Flow Rate

Applicable for Methods:

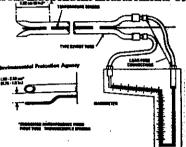
EPA Method 2, CARB 2, SCAQMD Method 2.1

Principle:

The average gas velocity in a stack gas is determined from the gas density and from measurement of the average velocity head with a type S or standard pitot tube.

Sampling Procedure:

Set up the apparatus as shown in the figure. Measure the velocity head and temperature at the traverse points specified by EPA Method 2, CARB Method 2 or SCAQMD Method 2.1. Measure the static pressure in the stack and determine the atmospheric pressure. The stack gas molecular weight is determined from independent measurements of O₂, CO₂ and H₂O concentrations.



Sample Recovery: and Analyses:

The stack gas velocity is determined from the measured average velocity head, the measured dry concentrations of O₂ and CO₂ and the measured concentration of H₂O. The velocity is determined from the following set of equations:

Where,

 ΔP = velocity head, inches in H_2O

Ts = gas/temperature, degrees R

Ps = absolute static pressure

Mwd = dry molecular weight

Mw = molecular weight

Cp = pitot flow coefficient

Dry molecular weight of stack gas

$$Mwd = 0.44 \ (\%CO_2) + 0.32 \ (\%O_2) + 0.28 \ (\%N_2 + \%CO)$$

Molecular weight of stack gas, wet basis

$$M_w = (M_{wd} \times M_d) + 18 (1 - M_d)$$

Where,
$$M_d = \frac{100 - Bws}{100}$$

Stack gas velocity

$$(V_s)$$
 avg.=(5130) $C_p \times \sqrt{\Delta}P$ avg. $\times \sqrt{T_s} \times (\frac{1}{P_s \times M_w})^{1/2}$

Determination of Moisture in Stack Gases

Applicable for Methods:

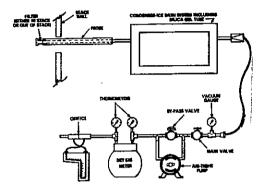
EPA Method 4, ARB 1-4, SCAQMD Method 4.1

Principle:

A gas sample is extracted at a constant rate from the source; moisture is removed from the stream and determined either volumetrically or gravimetrically.

Sampling Procedure:

Set up train as shown in the following figure. Sample is drawn at a constant rate through a sufficiently heated probe. The probe is connected to the impinger train by Teflon or glass tubing. The train consists of two greenburg smith impinger (SCAQMD 4.1) or one modified and 1 greenburg smith impinger (CARB & EPA) each containing 100 ml of water, an empty impinger as a knock-out and an impinger containing silica gel to protect the pump from moisture.



Sample Recovery: and Analyses:

Following testing, moisture content is determined gravimetrically or volumetrically from initial and final impinger contents weights or volume.

Determination of Particulate Matter Emissions From Stationary Sources Using a Wet Impingement Train

Reference:

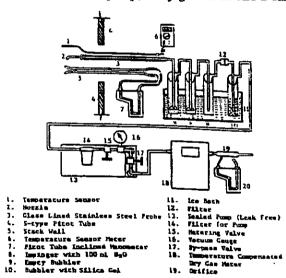
SCAQMD Method 5.1

Principle:

Stack gas is withdrawn isokinetically from the source through a sample train. Particulate matter is collected in impingers containing deionized water and on a back-up filter. The impingers are contained in an ice bath to maintain a sampled gas temperature of approximately 15° C (60° F). The filter is not heated.

Sampling Procedure:

The sampling train is shown in the figure below. The sample is drawn isokinetically through a glass or quartz probe (hi-temp). The probe is connected to an impinger train by Teflon tubing. The train consists of two Greenburg-Smith impingers which contain 100 ml of DI water; an empty impinger as a knock-out; and an impinger containing silica gel to protect the pump from moisture. Sample is withdrawn isokinetically from each predetermined sample point (determined using SCAQMD Method 1.1) through the sample train, which is followed by a vacuum line, a pump, a dry gas meter and a calibrated orifice.



Sample Recovery:

The moisture content is determined either gravimetrically or volumetrically from initial and final impinger weights or volume. Then the filter, probe/impinger rinse (including nozzle rinse, liner rinse, impinger contents and rinses) and silica gel are recovered into Containers #1, #2 and #3, respectively.

Analytical Procedure:

The aqueous sample is filtered through a tared fiberglass filter. An organic extraction is performed on the resulting solution using methylene chloride. Both the extraction filter and sample train filter are desiccated then measured gravimetrically. The organic extract and aqueous catch are evaporated, desiccated and measured gravimetrically.

If significant levels of sulfur compounds are present in the stack, each sample fraction is analyzed by acid-base titration for acid sulfate content and by barium-thorin titration for sulfate content.

Determination of Total Gaseous Non-Methane Organic Emissions as Carbon

Reference:

SCAOMD Method 25.1

Principle:

A sample of flue gas is drawn through a condensate trap and into an evacuated 12 liter tank. Volatile organic compounds (VOC), as total gaseous non-methane organics (TGNMO), are determined by combining results from independent analysis of condensate in the traps and gases in the tanks.

Sampling Procedure:

Duplicate gas samples are withdrawn from a source at a constant rate through condensate traps immersed in dry ice followed by evacuated 12 liter (nominal) tanks. Heavy organic components condense as liquids and solids in the condensate traps. Lighter components pass as gases through the traps into the tanks. The combined results from tanks and trap analyses are used to determine a qualitative and quantitative expression of the effluent gas stream. Duplicate sampling is designed into the system to demonstrate precision.

The sampling apparatus is checked for leaks prior to the sampling program by attaching the probe end to an absolute pressure gauge and vacuum pump in series. The sample lines were evacuated to less than 10 mm Hg and the gauge shutoff valve is then closed. The sample lines are deemed to be leak-free if no loss of vacuum occurs as indicated by the vacuum gauge. During sampling the tank pressures are monitored with a 0-30 inch vacuum gauge to ensure integrated sampling.

The final vacuum of each sample is measured using a slack tube manometer. The sample is then pressurized to 800 mm Hg absolute with ultrapure nitrogen. Each sample is then analyzed using the SCAQMD TCA procedure for total non methane hydrocarbons.

Analytical Procedure:

Condensate traps are analyzed by first stripping carbon dioxide (CO_2) from the trap. The organic contents are then removed and oxidized to CO_2 . This CO_2 is quantitatively collected in an evacuated vessel and measured by injection into a flame ionization detection/total combustion analysis (FID/TCA) system.

The organic content of the sample fraction collected in each tank is measured by injecting a portion into the FID/TCA analysis system which uses a two phase gas chromatography (GC) column to separate carbon monoxide (CO), methane (CH₄) and carbon dioxide (CO₂) from each other and from the total gaseous nonmethane organics (TGNMO) which are eluted as backflush. All eluted components are first oxidized to CO₂ by a hopcalite catalyst and then reduced to methane by a nickel catalyst. The resulting methane is detected using the flame ionization detector. A gas standard containing CO, CH₄, CO₂ and propane, traceable to NBS, is used to calibrated the FID/TCA analysis system.

Determination of Total Gaseous Non-Methane Organic Emissions as Carbon

Reference:

SCAQMD Method 25.3

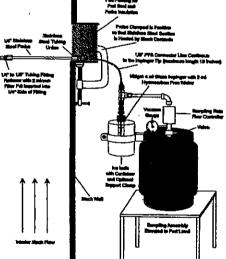
Principle:

A sample of flue gas is drawn through a condensate trap (mini-impinger) and into an evacuated six liter SUMMA canister. Volatile organic compounds (VOC), as total gaseous non-methane organics (TGNMO), are determined by combining results from independent analysis of condensate in the traps and gases in the SUMMA canisters.

Sampling Procedure:

Duplicate gas samples are withdrawn from a source at a constant rate through condensate traps immersed in an ice bath followed by evacuated six liter (nominal) SUMMA canisters. Heavy organic components condense as liquids and solids in the condensate traps. Lighter components pass as gases through the traps into the canisters. The combined results from canisters and mini-impinger analyses are used to determine a qualitative and quantitative expression of the effluent gas stream. Duplicate sampling is designed into the system to demonstrate precision.

The sampling apparatus is checked for leaks prior to the sampling program by capping the end of the sample probe. The sample flow valve is then opened and then closed to introduce vacuum to the system. The vacuum drop should then cease numerically above 10 in. Hg. A cease in movement of the vacuum gauge for a period of ten minutes indicates an acceptable leak check. When sampling is initiated, the vacuum gauge must indicate a canister vacuum of greater than 28 in. Hg. Immediately after sampling a post-test leak check is performed, followed by a rinse of the PFA line into the condensate trap with 0.5 to 1.0 ml of hydrocarbon free water.



Analytical Procedure:

Condensate traps are analyzed for total organic carbon by liquid injection into an infrared total organic carbon analyzer.

The organic content of the sample fraction collected in each canister is measured by injecting a portion into the FID/TCA analysis system which uses a two phase gas chromatography (GC) column to separate carbon monoxide (CO), methane (CH₄) and carbon dioxide (CO₂) from each other and from the total gaseous non-methane organics (TGNMO) which are eluted as backflush. All eluted components are first oxidized to CO₂ by a hopcalite catalyst and then reduced to methane by a nickel catalyst. The resulting methane is detected using the flame ionization detector. A gas standard containing CO, CH₄, CO₂ and propane, traceable to NBS, is used to calibrated the FID/TCA analysis system.

CONTINUOUS EMISSIONS MONITORING SYSTEM - TRUCK

SCAQMD Method 100.1

The continuous emissions monitoring system consists of a Thermo Electron Model 10AR chemiluminescence NO/NO_X analyzer, a Teledyne electro chemical O₂ analyzer, a Thermo Electron Model 48H CO gas filter correlation analyzer and a Horiba PIR 2000 non dispersive infrared CO₂ analyzer. All analyzer specifications are provided in Table 1. All concentrations are determined on a dry basis. Concentrations of NO_X, CO, O₂ and CO₂ are continuously recorded on a Linseis 10-inch strip chart recorder and a Strawberry Tree Data Acquisition System (DAS). The extractive monitoring system conforms with the requirements of SCAQMD Method 100.1.

The sampling probe (heated to 250°F), constructed of 1/2 inch-diameter 316 stainless steel, is connected to a condenser with a six foot length of 3/8 inch Teflon line (heated to 250°F). A Nupro stainless steel filter (10 micron) is connected at the tip of the probe and maintained at stack temperature.

The condenser consists of a series of two stainless steel moisture knock-out bottles immersed in an ice water bath. The system is designed to minimize contact between the sample and the condensate. Condensate is continuously removed from the knock-out bottles via a peristaltic pump. The condenser outlet temperature is monitored either manually at 10-minute intervals or on a strip chart recorder/DAS system. The sample exiting the condenser is then transported through a filter, housed in a stainless steel holder, followed by 3/8 inch O.D. Teflon tubing and a Teflon coated (or stainless steel/viton) diaphragm pump to the sample manifold. The sample manifold is constructed of stainless steel tubing and directs the sample through each of five rotameters to the NO_X monitor, O₂ monitor, CO monitor, CO₂ monitor and excess sample exhaust line, respectively. Sample flow through each channel is controlled by a back pressure regulator and by stainless steel needle valves on each rotameter. All components of the sampling system that contact the sample are composed of stainless steel, Teflon or glass.

The calibration system is comprised of two parts: the analyzer calibration and the system bias check. The calibration gases are, at a minimum, certified to \pm 1% by the manufacturer. Where necessary to comply with the reference method requirements, EPA Protocol 1 gases are used. The cylinders are equipped with pressure regulators which supply the calibration gas to the analyzers at the same pressure and flow rate as the sample. The selection of zero, span or sample gas directed to each analyzer is accomplished by operation of the zero, calibration or sample selector knobs located on the main flow control panel.

For SCAQMD Method 100.1 testing, the following procedures are conducted before and after each series of test runs:

Leak Check:

The leak check is performed by plugging the end of the sampling probe, evacuating the system to at least 20 inches of Hg. The leak check is deemed satisfactory if the system holds 20 inches of Hg vacuum for five minutes with less than one inch Hg loss.

Linearity Check:

The NO_x , CO, CO_2 and O_2 analyzers linearity check is performed by introducing, at a minimum, zero gas, mid range calibration gas (40-60% scale) and high range calibration gas (80-100% scale). Instrument span value is set on each instrument with the mid range gas. The high range calibration gas (80-100% scale) is then introduced into each instrument without any calibration adjustments. Linearity is confirmed, if all values agree with the calibration gas value to within 2% of the range.

Stratification Check:

A stack stratification check is performed (pre-test only) by traversing the stack comparing four traverse points to the reference point (center). If the gas composition is homogenous, <10% variation between any traverse points in the gas stream and the reference point. Single point gas sampling is performed at the reference point. If stratification exceeds the 10% criteria, then the stack cross section is traversed during sampling.

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System Bias Check:

The system bias check is accomplished by transporting the same gases used to zero and span the analyzers to the sample system as close as practical to the probe inlet. This is accomplished by opening a valve located on the probe, allowing the gas to flow to the probe and back through the moisture knockout and sample line to the analyzers. During this check the system is operated at the normal sampling rate with no adjustments. The system bias check is considered valid if the difference between the gas concentration exhibited by the measurement system which a known concentration gas is introduced at the sampling probe tip and when the sample gas is introduced directly to the analyzer, does not exceed \pm 5% of the analyzer range.

Response Time:

Response time (upscale and downscale) for each analyzer is recorded during the system bias check. Upscale response time is defined as the time it takes the subject analyzer gas to reach 95% of the calibration gas value after introducing the upscale gas to the sample bias calibration system. Downscale response time is defined as the time it takes the subject analyzer to return to zero after the zero gas is introduced into the sample system bias calibration system.

NO. Conversion Efficiency

The NO_x analyzer NO_2 conversion efficiency is determined by injecting a NO_2 gas standard directly into the NO_x analyzer (after initial calibration). The analyzer response must be a least 90% of the NO_2 standard gas value.

NO₂ Converter Efficiency (alternate method)

The mid level NO gas standard is directly injected into a clean leak-free Tedlar bag. The bag is then diluted 1:1 with air (20.9 % O_2). The bag is immediately attached to the NO_x sample line. The initial NO_x concentration is recorded on the strip chart. After at least 30 minutes the Tedlar bag is reattached to the NO_x sample line. Analyzer response must be at 98% of the initial Tedlar bag NO_x value to be acceptable.

In between each sampling run the following procedures are conducted:

Zero and Calibration Drift Check:

Upon the completion of each test run, the zero and calibration drift check is performed by introducing zero and mid range calibration gases to the instruments, with no adjustments (with the exception of flow to instruments) after each test run. The analyzer response must be within \pm 3% of the actual calibration gas value.

Analyzer Calibration:

Upon completion of the drift test, the analyzer calibration is performed by introducing the zero and mid range gases to each analyzer prior to the upcoming test run and adjusting the instrument calibration as necessary.

System Bias Check

(same as above)

A schematic of the sample system and specific information of the analytical equipment is provided in the following pages.

TABLE 1

CONTINUOUS EMISSIONS MONITORING LABORATORY - TRUCK

NO_x CHEMILUMINESCENT ANALYZER -- THERMO ELECTRON MODEL 10 A

Response Time (0-90%)

1.5 sec -- NO mode/1.7 sec -- NO_x mode

Zero Drift

Negligible after 1/2 hour warmup

Linearity

±1% of full scale

Accuracy

Derived from the NO or NO₂

calibration gas, ± 1% of full scale

Operating Ranges (ppm)

2.5, 10, 25, 100, 250, 1000, 2500, 10000

Output

0-1 volt

O₂ ANALYZER, FUEL TYPE -- TELEDYNE MODEL 326RA

Response Time (0-90%)

60 seconds

Accuracy

 \pm 1% of scale at constant temperature \pm 1% of scale of \pm 5% of reading.

 \pm 1% of scale of \pm 5% of reading, whichever is greater, over the operation

temperature range.

Operating Ranges (%)

0-5, 0-25

Output

0-1 volt

O₂ ANALYZER, PARAMAGNETIC -- SERVOMEX MODEL 1400B

Response Time (0-90%)

15 seconds

Accuracy

0.1% oxygen

Linearity

 \pm 1% scale

Operating Ranges (%)

0-25, 0-100

Output

0-1 volt

CO GAS FILTER CORRELATION -- THERMO ELECTRON MODEL 48H

Response Time (0-95%)

1 minute

Zero Drift

+ 0.2 ppm CO

Span Drift

Less than 1% full scale in 24 hours

Linearity

± 1% full scale, all ranges

Accuracy

 ± 0.1 ppm CO

Operating Ranges (ppm)

50, 100, 250, 500, 1000, 2500, 5000,

10,000, 25,000, 50,000

Output

0-1 volt

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TABLE 1 (Cont.)

CO2 INFRARED GAS ANALYZER -- HORIBA - MODEL PIR 2000

Response Time (0-90%) 5 seconds

Zero Drift \pm 1% of full scale in 24 hours Span Drift \pm 1% of full scale in 24 hours

Linearity $\pm 2\%$ of full scale

Resolution Less than 1% of full scale

Operating Ranges (%) 0-5, 0-15, 0-25

Output 0-1 volt

SO₂ PULSED FLOURESCENT - TECO - MODEL 43C-HL

Response Time80 secondsZero Drift $\pm 1\%$ Span Drift $\pm 1\%$ Linearity $\pm 1\%$ Resolution $\pm 1\%$

Operating Ranges 5, 10, 20, 50, 100, 200, 500, 1000, 2000, 5000

Output 0-10 volt

RATFISCH FID TOTAL HYDROCARBON ANALYZER -- MODEL 55CA

Response Time (0-90%) 5 seconds

Zero Drift $\pm 1\%$ full scale in 24 hours Span Drift $\pm 1\%$ full scale in 24 hours Linearity $\pm 1\%$ full scale - constant

Accuracy $\pm 1\%$ full scale at constant temp.

Operating Ranges (ppm) 10, 100, 1000, 10,000

Output 0 - 10 volts

LINSEIS MODEL L2045 FOUR PEN STRIP CHART RECORDER

Pen Speed up to 120 cm/min

Measuring Response 0-20 volts
Linearity Error 0.25%
Accuracy 0.3%

Zero Suppression Manual (from 1 to 10X full scale)

LINEAR 3 PEN CONTINUOUS -- MODEL 595 STRIP CHART

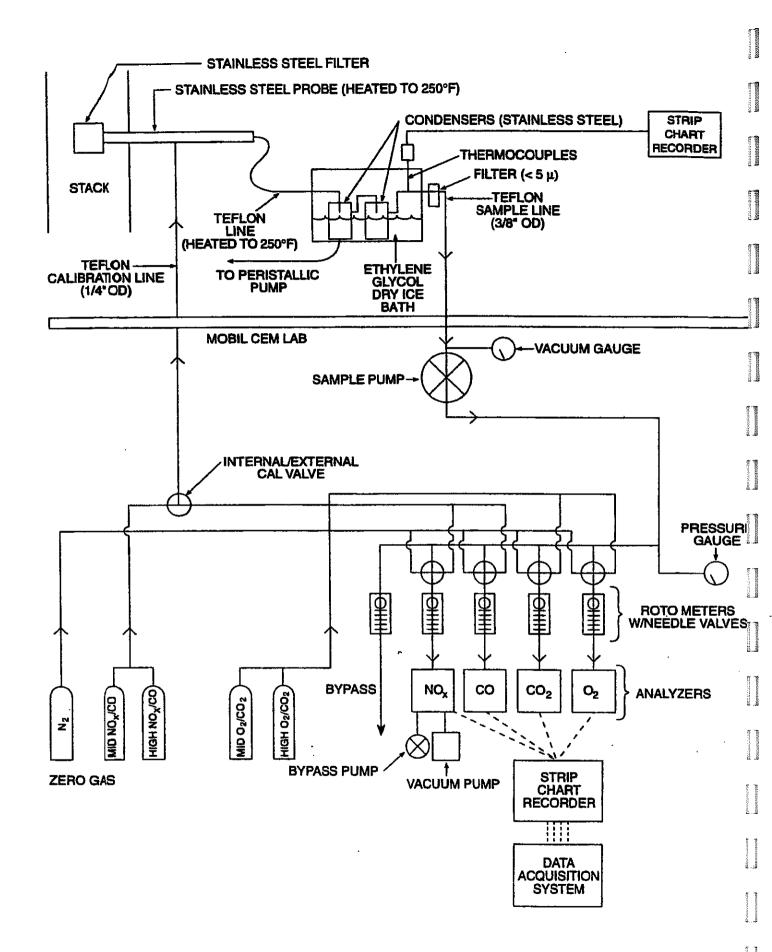
Pen Response 20 inches/second Measuring Response 1 Mv through 5V

Zero Set Electronically adjustable full scale with 1 full

scale of zero suppression

Accuracy Total limit of error $\pm 0.5\%$

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NO/NO_x by Continuous Analyzer

Applicable Reference

Methods:

EPA 7E, EPA 20; CARB 100, BAAQMD ST-13A, SCAQMD 100.1

Principle:

A sample is continuously withdrawn from the flue gas stream, conditioned and conveyed to the instrument for direct readout of NO or NO_x .

Analyzer:

TECO Model 10AR

Measurement Principle:

Chemiluminescence

Accuracy:

1% of full scale

Ranges:

0-2.5, 0-10, 0-25, 0-100, 0-250, 0-1000, 0-2500, 0-10,000 ppm

Output:

0-10 V

Inferences:

Compounds containing nitrogen (other than ammonia) may cause interference.

Response Time:

90%, 1.5 seconds (NO mode) and 1.7 seconds (NO $_{\! X}$ mode)

Sampling Procedure:

A representative flue gas sample is collected and conditioned using the CEM system described previously. If EPA Method 20 is used, that method's specific procedures for selecting sample points are used.

Analytical Procedure:

The oxides of nitrogen monitoring instrument is a chemiluminescent nitric oxide analyzer. the operational basis of the instrument is the chemiluminescent reaction of NO and ozone (O₃) to form NO₂ in an excited state. Light emission results chemiluminescence is monitored through an optical filter by a high sensitivity photomultiplier tube, the output of which is electronically processed so it is linearly proportional to the NO concentration. The output of the instrument is in ppmV.

When NO_2 is expected to be present in the flue gas, a supercooled water dropout flask will be placed in the sample line to avoid loss of NO_2 . Since NO_2 is highly soluble in water, "freezing out" the water will allow the NO_2 to reach the analyzers for analysis. The analyzer measures NO_2 only. In the NO_2 mode, the gas is passed through a moly converter which converts NO_2 to NO_2 and a total NO_2 measurement is obtained. NO_2 is determined as the difference between NO_2 and NO_3 . Use of a moly converter instead of a stainless steel converter eliminates NH_3 interference; NH_3 is converted to NO_3 with a stainless converter, but not with a moly converter.

Method: Oxygen (O₂) by Continuous Analyzer

Applicable Reference EPA 3A, EPA 20, CARB 100, BAAQMD ST-14, SCAQMD 100.1

Methods:

Principle: A sample is continuously withdrawn from the flue gas stream, conditioned and conveyed to the instrument for direct readout of O_2 concentration.

Analyzer: Teledyne Model 326R

Measurement Principle: Electrochemical cell

Ranges: 0-5, 0-25% 0-100%

Accuracy: 1% of full scale

Output: 0-1 V

Interferences: Halogens and halogenated compounds will cause a positive interference.

Acid gases will consume the fuel cell and cause a slow calibration drift.

Response Time: 90% < 60 seconds

Sampling Procedure: A representative flue gas sample is collected and conditioned using the

CEM system described previously. If Method 20 is used, that method's specific procedures for selecting sample points are used. Otherwise, stratification checks are performed at the start of a test program to select

single or multiple-point sample locations.

Analytical Procedure: An electrochemical cell is used to measure O_2 concentration. Oxygen in the

flue gas diffuses through a Teflon membrane and is reduced on the surface of the cathode. A corresponding oxidation occurs at the anode internally and an electric current is produced that is proportional to the concentration of oxygen. This current is measured and conditioned by the instrument's

electronic circuitry to give an output in percent O₂ by volume.

Method: Carbon Dioxide (CO2) by Continuous Analyzer EPA 3A, CARB 100, BAAQMD ST-5, SCAQMD 100.1 Applicable Reference A sample is continuously drawn from the flue gas stream, conditioned and Principle: conveyed to the instrument for direct readout of CO₂ concentration. Analyzer: PIR 2000 Measurement Principle: Non-dispersive infrared (NDIR) Accuracy: 1% of full scale Ranges: 0-5, 0-15% Output: 0-1 V A possible interference includes water. Since the instrument receives dried Interferences: sample gas, this interference is not significant. Response Time: 5 seconds Sampling Procedure: A representative flue gas sample is collected and conditioned using the CEM system described previously. Carbon dioxide concentrations are measured by short path length non-Analytical Procedure: dispersive infrared analyzers. These instruments measure the differential in infrared energy absorbed from energy beams passed through a reference cell (containing a gas selected to have minimal absorption of infrared energy in the wavelength absorbed by the gas component of interest) and a sample cell through which the sample gas flows continuously. differential absorption appears as a reading on a scale of 0-100%.

Method:

Carbon Monoxide (CO) by NDIR/Gas Filter Correlation

Applicable Reference Methods:

EPA 6C; CARB 1-100; BAAQMD ST-6, SCAQMD 100.1

A sample is continuously drawn from the flue gas stream, conditioned and conveyed to the instrument for direct readout of CO concentration.

Analyzer:

TECO, Model 48H

Measurement Principle:

NDIR/Gas Filter Correlation

O.1% ppm

Output: 0-1 V

Ranges:

Sampling Procedure:

Analytical Procedure:

ppm

Interferences: Negligible interference from water and CO₂

Rise/Fall times (0-95%) 1 minute @ 1 lpm flow, 30 second integration time

A representative flue gas sample is collected and conditioned using the CEM system described previously. Sample point selection has been described previously.

0-50, 0-100, 0-250, 0-500, 0-1000, 0-2500, 0-5000, 0-10000, 0-2500, 0-3,000

Radiation from an infrared source is chopped and then passed through a gas fill r which alternates between CO and N_2 due to rotation of a filter wheel. The radiation then passes through a narrow band-pass filter and a multiple optical personal sample cell where absorption by the sample gas occurs. The IR radiation exists the sample cell and falls on a solid state IR detector.

Method: Sulfur Dioxide (SO₂) by Pulsed Flourescent Applicable Reference EPA 10; CARB 1-100; BAAQMD ST-6, SCAOMD 100.1 Methods: Principle: A sample is continuously drawn from the flue gas stream, conditioned and conveyed to the instrument for direct readout of SO₂ concentration. Analyzer: TECO, Model 43C-HL Measurement Principle: Pulsed flourescense SO₂ analyzer Precision: 0.1% ppm Ranges: 5, 10, 20, 50, 100, 200 ppm Output: 0-10 V Less than lower detectable limit except for the following: NO <3 ppb, m-xylene Interferences: <2 ppm, H₂O <2% of reading. Response Time: 80 seconds Sampling Procedure: A representative flue gas sample is collected and conditioned using the CEM system described previously. Sample point selection has been described previously. Analytical Procedure: The sample flows into the flourescent chamber, where pulsating UV light excites the SO₂ molecules. The condensing lens focuses the pulsating UV light into the mirror assembly. The mirror assembly contains four selecting mirrors that reflect only the wavelengths which excite SO₂ molecules. As excited SO₂ molecules decay to lower energy states they emit UV light that is proportional to The PMT (photomultiplier tube) detects UV light the SO₂ concentration. emission from decaying SO₂ molecules. The PMT continuously monitors pulsating UV light source and is connected to a circuit that compensates for fluctuating in the light.



Atm AA inc.

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environmental consultants laboratory services

Tandem Gas Chromatographic/Mass Spectroscopic-Electrolytic Conductivity Detector (GC/MS-ELCD) Method for Determination of Total Sulfur in Gas Samples

AtmAA, Inc. 03-060

3/30/93

This method measures selected reduced sulfur species, including but not limited to hydrogen sulfide, carbonyl sulfide, mercaptan, ethyl mercaptan, dimethyl sulfide, carbon disulfide, isopropyl mercaptan, n-propyl mercaptan, and dimethyl disulfide in qaseous sample matrices using gas chromatographic separation and a mass spectrometric and electrolytic conductivity detector (ELCD), where the ELCD measures hydrogen sulfide only. A non-polar methyl silicon capillary gas chromatographic column is used for component separation and selected ion monitoring is used for component Component quantification is obtained using a quantification. multi-component external standard prepared by Scott Specialty The lower detection limit varies by component but is at least 0.1 ppmv ethyl mercaptan (component of lowest sensitivity) for a 0.31 ml sample volume injection. The upper quantitation limit has not been determined but is at least beyond 80 ppmv dimethyl disulfide, for which response remained linear from 0.1 ppmv to 80 ppmv.

Hydrogen sulfide is measured using an electrolytic conductivity detector operated in the oxidative sulfur mode. A Chromosil 310 column, operated isothermally at 45°C. is used to separate $\rm H_2S$ from other sulfur components. A fixed volume loop injection is used in the analysis for $\rm H_2S$.

Lower Detection Limits (LDL's):

Using a 1 ml injection volume for H₂S by electrolytic conductivity detector and 0.40 ml injection volume for GC/MS measured sulfur compounds, the following LDL's are obtained:

	(ppmv)
Hydrogen sulfide	0.5
Carbonyl sulfide	0.03
Methyl mercaptan	0.03
Ethyl mercaptan	0.04
Dimethyl sulfide	0.02
Carbon disulfide	0.02
i-propyl mercaptan	0.03
n-propyl mercaptan	0.03
Dimethyl disulfide	0.02

Equipment:

A Hewlett-Packard 5890 series II gas chromatograph (GC), Hewlett-Packard 5971A Mass Selective Detector, 486 MS/DOS computer and HP operating software are used for all sulfur species except H₂S. The GC is fitted with a heated 6-port Valco 1/16" line, sample injection valve. All gas transfer lines to the sample loop are fused silica lined Restek tubing. The fixed volume (0.40 ml) sample loop is Teflon. The transfer line from the valve to the GC column is cleaned and treated blank 0.53 mm OD fused silica line with polyimide coating.

 $\rm H_2S$ is measured using a Varian 1400 GC with the Hall oxidative quartz tube furnace and electrolytic cell attached. Nitrogen is used as carrier and oxygen is used as the combustion gas.

Multi-component gaseous standards are prepared by Scott Specialty Gas and are contained in two separate aluminum cylinders and a Scotty IV canister as follows:

Cylinder A (CAL12250)		Cylinder B (CAL	3563)
Carbonyl sulfide Ethyl mercaptan Carbon disulfide	15.2 ppmv 13.4 ppmv 16.1 ppmv	Hydrogen sulfide Methyl mercaptan Dimethyl sulfide Dimethyl disulfide	12.3 ppmv 22.6 ppmv 20.3 ppmv

Scotty IV (mix 252)

Hydrogen Sulfide 93.8 ppmv

Gas tight clean glass volumetric syringes of 10, 20, & 50 ml capacity, with smooth glass barrel (not sintered glass) are used to make volumetric dilutions of sample or standard.

GC/MS SIM parameters:

Dwell per ion	start time	Ions		
Group 1: 75 msec. Group 2: 75 msec. Group 3: 75 msec. Group 4: 75 msec.	8.0 min. 10.0 min. 14.5 min. 19.5 min.	60 47,48,64 47,62,76,78,43,61 79,94,122,142,156, 128		

Components monitored:

Group 1: carbonyl sulfide Group 2: methyl mercaptan

Group 3: ethyl mercaptan, dimethyl disulfide, carbon

disulfide, isopropyl mercaptan, n-propyl mercaptan

Group 4: dimethyl sulfide

Component	Quantitation ion		Confirmation	ion
carbonyl sulfide	60		none	and the same of th
methyl mercaptan	47		48	ij B
ethyl mercaptan	62		47	8°3
dimethyl sulfide	62		47	TO STATE OF THE PERSON NAMED IN COLUMN NAMED I
carbon disulfide	76		78	2
iso-propyl mercapta	n 76		43,47,61	_
n-propyl mercaptan	76	•	43,47,61	Strange
dimethyl disulfide	94 .	•	79	

Sulfur dioxide is analyzed by monitoring mass 64 which is included in Group 2 ions.

Calibration:

Gaseous standards can be analyzed prior to or after a set of samples. Response factors are determined from a single point standard calibration. Multi-point calibrations are performed to verify linearity. Consistency of standard response with continuing calibrations is observed to indicate performance of multi-point calibration.

Samples containing components at less than the stated LDL can be analyzed by cryogenically focusing a measured volume of gaseous sample onto a glass bead filled Teflon loop immersed in liquid argon. The sample is thermally transferred upon injection by immersing the sample loop in near boiling temperature water. The LDL obtained by this technique is calculated as:

 $LDL_{cryo} = (cryo volume/0.40)*LDL_{o.40}$

Acceptable volumes for cryogenic concentration range from 3 to 10 ml. and are determined based on amounts of other components in the sample such as water, carbon dioxide or hydrocarbons.

Procedure:

A volumetric sample of landfill or source collected gas intransferred from a Tedlar bag to the 6-port valve injection linusing a glass syringe of approximately 10 ml. A Teflon loop of 0.40 ml volume is used to inject the sample. When sample concentrations exceed that of the standard, appropriate volumetric sample dilutions are made using the glass syringes with dry nitrogen diluent. Immediately after sample injection, the GC/MS is started. Standards are analyzed in the same manner as samples appropriate component peaks are monitored and integrated after sample analysis data set has been obtained.

Hydrogen sulfide is measured using the electrolytic conductivit detector by a separate direct fixed loop valve injection using heated Teflon loop, transfer lines, and Teflon Chromosil 310 GC column.



A response factor for a standard component is calculated as:

rf = std. amt. / std. area

Sample concentration is calculated using the response factor:

conc. = rf x sample area

At least 10% of samples in a sample set, or minimum of one sample per set are analyzed twice to determine precision. A separate report showing repeat analyses results is included with an analytical report of sulfur component concentrations per each sample set. Repeat analyses must agree within +/- 10% except for component concentrations less than 1 ppmv. A nitrogen blank is analyzed between standards and samples to verify that there is no component carry-over. Samples are analyzed as soon after they are ived as possible, preferably same day and within four hours of

ection. Data is being gathered to determine stability of sulfur compounds in Tedlar bag containers in an effort to extend sample holding time. Samples are usually analyzed before standards to prevent carry-over, since most sulfur components measured in landfill gas samples are lower in concentration than those in the standards.

GC/MS Analysis Conditions:

GC conditions: a 30 M \times 0.2 mm, 0.50 um film methyl silicon PONA column from Hewlett-Packard is temperature programmed as follows:

-65 degrees C, hold min. 15 degrees C min. to 220 degrees C, hold 5 min.

Valve oven Temp. 150 degrees C GC/MS transfer line 180 degrees C Carrier gas is helium, pressure regulated at 21 psi.

MS Conditions:

MS calibration is performed periodically prior to performing analyses using PFTBA (perfluoro-tributylamine) as supplied by Hewlett-Packard and as controlled by HP software under the mid-range auto time program. Solvent delay = 8 min.

Hall Detector/GC Analysis Conditions:

6' x 1/8" Teflon, Chromosil 310 analytical column 45 degrees C, isothermal Valve oven & transfer line Temp. 105 degrees C. Carrier gas is nitrogen, flow rate 18 cc/min. Oxygen oxidation gas, flow rate 18 cc/min. Quartz tube oxidation oven Temp. 650 degrees C.



Hydrocarbons by SCAQMD Micro Total Carbon Analyses

Reference:

Tedlar Bag Lung Sampler

Principle:

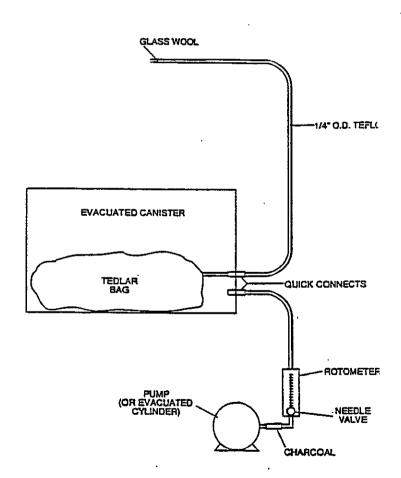
Duplicate Tedlar bags are filled with flue gas at a constant rate. The bag contents are analyzed by total combustion analyses/flame ionization detection for methane and total gaseous non-methane hydrocarbons.

Sampling Procedure:

Duplicate samples are collected by evacuating the canister (see figure) at a constant rate over each test run using a rotameter/needle valve and a diaphragm pump. Prior to each sampling run, the evacuated canister (containing the Tedlar bag) is leak checked at 2" Hg vacuum. The sample train upstream of the Tedlar bag is then purged with stack gas. At the conclusion of each test run, each Tedlar bag sample is sealed and stored in an opaque container pending analysis.

Analytical Procedure:

Methane and TNMHC concentration from both samples are determined using the SCAQMD Total Combustion Analysis (TCA) procedure.



APPENDIX B - Computer Printout of Results

Facility: Bradley Landfill

Source: Flare #1 Job No.: W07-035 Date: 04/23/03

TOTAL COMBUSTION ANALYSIS RESULTS

Sample ID	Inlet 1A	Inlet 1B	Average
Run Number	IA	10	Avelage
Methane in Tank	391000	390000	390500
TNMHC, Tank (Noncond.)	856	838	
TNMHC - Condensables	8917.1	9763.3	
TNMHC - Total	9773.1	10601.3	
CO Concentration (ppm)	52.3	54.5	53.4
CO2 Concentration (ppm)	337000	333000	335000
O2 Concentration (%)	2.69	2.95	2.82
Sample Parameters			
Tank Number	Α	D	
Trap Number	R	0	
Sample Tank Volume (I)	12.202	12.051	
Initial Pressure (Torr)	2.5	2.5	
Initial Temperature (deg. K)	292	292	
Final Pressure (mm Hg)	455	437	
Final Temperature (deg. K)	292	292	
Sample Volume (I)	7.29	6.92	
Analysis Pressure (mm Hg)	800	800	
Analysis Temperature (deg. K	292	292	
ICV Volume (I)	2.266	2.266	
ICV Final Pressure (mm Hg)	800	800	
ICV Final Temperature (deg.	292	292	
CO2 in ICV (ppm)	28700	29800	
TNMHC, Trap (Condensables)	8917	9763	
Stack Total TNMHC	9773	10601	10187

NOTE: All hydrocarbon values are in terms of ppm, v/v, as methane.

SCAQMD Methods 1-4 Flowrate Determination

Facility: Bradley Landfill Source: Flare #1 Job No.: W07-035 Date: 04/23/03				
STANDARD TEMPERATURE	Degrees F	60		
RUN NUMBER CLOCK TIME: INITIAL CLOCK TIME: FINAL	***** *****	1 1012 1112	2 1153 1253	Average
AVG. STACK TEMPERATURE AVG. SQUARE DELTA P BAROMETRIC PRESSURE SAMPLING TIME SAMPLE VOLUME AVG. METER TEMP. AVG. DELTA H DGM CALIB. FACTOR [Y] WATER COLLECTED CO 2 CO CH4 N 2 STACK AREA STATIC PRESSURE PITOT COEFFICIENT SAMPLE VOLUME DRY WATER AT STD. MOISTURE MOLE FRACTION DRY GAS MOLECULAR WT. DRY EXCESS AIR MOLECULAR WT. WET STACK VELOCITY VOLUMETRIC FLOWRATE, DRY STD VOLUMETRIC FLOWRATE, ACTUAL	Degrees F Inches H20 Inches HG Minutes Cubic Feet Degrees F Inches H20 ****** Milliliters Percent Percent Percent Percent Square Inches Inches WG ****** DSCF SCF Percent Ib/Ib Mole Percent Ib/Ib Mole Inches HG AFPM DSCFM ACFM	141 1,0559 29.17 60 46.845 78.8 1,70 0,9873 52 33.5 2.8 0.0 39.1 24.6 137.9 10.00 0,99 43.70 2.5 5.3 0,95 28.79 77 28.21 29.91 4526 3549 4334	143 1.0593 29.17 60 46.815 86.4 1.70 0.9873 65 33.5 2.8 0.0 39.1 24.6 137.9 10.00 0.99 43.07 3.1 6.6 0.93 28.79 77 28.07 29.91 4560 3514 4367	142 1.0576 29.17 60 46.830 82.6 1.70 0.9873 59 33.5 2.8 0.0 39.1 24.6 137.9 10.00 0.99 43.39 2.8 6.0 0.94 28.79 77 28.14 29.91 4543 3531 4350
EMISSION RATES				
SAMPLE A TNMHC Concentration, as CH4 TNMHC Concentration, as CH4 TNMHC Emission Rate, as CH4	ppm mg/dscf lb/hr	9773 187 87.7		9773 187 87.2
SAMPLE B TNMHC Concentration, as CH4 TNMHC Concentration, as CH4 TNMHC Emission Rate, as CH4	ppm mg/dscf lb/hr	10601 203 95.1		10601 203 94.6
AVERAGE TNMHC Concentration, as CH4 TNMHC Concentration, as CH4 TNMHC Emission Rate, as CH4	ppm mg/dscf lb/hr	10187 195 91.4		10187 195 90.9

Facility: Bradley Landfill

Source: Flare #1 Job No.: W07-035 Date: 04/23/03

Sulfur Compounds

Speciated Compound		Concentration ppm, as H2S	No. of S molecules in Compound	Total S ppm, as H2S i	SO2 Conc. mg/dscf	Avg. Inlet Flow Rate dscfm	SO2 Rate lb/hr
Hydrogen Sulfide		48.4	1	48.40	3.706	3531	1.731
Carbonyl Sulfide		0.42	1	0.42	0.032	3531	0.015
Methyl mercaptan		3.16	1	3.16	0.242	3531	0.113
Ethyl mercaptan	<	0.09	1	0.09	0.007	3531	0.003
Dimethyl sulfide		9.50	1	9.50	0.727	3531	0.340
Carbon disulfide		0.22	2	0.44	0.034	3531	0.016
Dimethyl disulfide		0.220	2	0.44	0.034	3531	0.016
iso-propyl mercaptan		0.28	1	0,28	0.021	3531	0.010
n-propyl mercaptan	<	0.06	1	0.06	0.005	3531	0,002
Total				62.79			2.246

EXPANSION AND F-FACTOR CALC. METHOD

 Client:
 Bradley Landfill
 Date:
 04/23/03

 Location:
 Sun Valley, CA
 Job #:
 W07-035

 Unit:
 Flare #1
 Run#:
 1

Fuel temperature deg. F Std. Temp. 60 deg. F
Fuel Pressure psi
Fuel Flow Rate cfm Fuel Flow 3549 dscfm
Exhaust Outlet O2 13.78 %

Barometric Pressure 29.17

COMPONENTS		MOLE %	HHV btu/ft3	LLV btu/ft3	Exp Factor dscf/scf fue
Oxygen	ſ	2.82			0.028
Nitrogen		24.62			0.246
Carbon Dioxide	Ì	33.50			0.335
Methane	1	39.05	394.41	355.12	3.347
Ethane	C2		0.00	0.00	0.000
Propane	СЗ		0.00	0.00	0.000
Iso-Butane	C4		0.00	0.00	0.000
N-Butane			0.00	0.00	0.000
Iso-Pentane	C5		0.00	0.00	0.000
N-Pentane			0.00	0.00	0.000
Hexane	C6		0.00	0.00	0.000
Heptane	C7		0.00	0.00	0.000
Octane	C8		0.00	0.00	0.000
Nonane	C9		0.00	0.00	
Total		99.99	394.41	355.12	3.96

CALCULATIONS

EXHAUST FLOW RATE, Q = (scfm*Exp Fac)*(20.92(20.92-%O2)

41134 DSCFM

EPA F-Factor = (scf exhaust/scf fuel)/(btu/scf fuel)*(1000000 btu/MMbtu)

10030 dscf/Mmbtu

EXPANSION AND F-FACTOR CALC. METHOD

 Client:
 Bradley Landfill
 Date:
 04/23/03

 Location:
 Sun Valley, CA
 Job #:
 W07-035

 Unit:
 Flare #1
 Run#:
 2

Fuel temperature	deg. F	Std. Temp.	<u>60</u> deg. F
Fuel Pressure Fuel Flow Rate	psi cfm	Fuel Flow	3514 dscfm
Exhaust Outlet O2	14.24 %		
Barometric Pressure	<u>29.17</u>		

COMPONENTS	i	MOLE %	HHV btu/ft3	LLV btu/ft3	Exp Factor dscf/scf fue
					0.000
Oxygen	L	2.82			0.028
Nitrogen		24.62			0.246
Carbon Dioxide	<u> </u>	33.50			0.335
Methane	r	39.05	394.41	355.12	3.347
Ethane	C2		0.00	0.00	0.000
Propane	СЗ	1	0.00	0.00	0.000
Iso-Butane	C4	i	0.00	0.00	0.000
N-Butane	-·	Ì	0.00	0.00	0.000
Iso-Pentane	C5		0.00	0.00	0.000
N-Pentane	~~		0.00	0.00	0.000
Hexane	C6		0.00	0.00	0.000
* * * * * * * * * * * * * * * * * * * *	C7		0.00	0.00	0.000
Heptane	C8		0.00	0.00	0.000
Octane			0.00	0.00	
Nonane	C9 [0.00	0.00	
Total		99.99	394.41	355.12	3.96

CALCULATIONS

EXHAUST FLOW RATE, Q = (scfm*Exp Fac)*(20.92(20.92-%O2)

43527 DSCFM

EPA F-Factor = (scf exhaust/scf fuel)/(btu/scf fuel)*(1000000 btu/MMbtu)

10030 dscf/Mmbtu

SCAQMD Method 5.1 Particulate Emissions

Facility:	Bradley Landfill
Source:	Flare #1
Joh No.:	W07-035

Date: (

04/23/03

STANDARD TEMPERATURE	Degrees F	60			
RUN NUMBER	*****	1	2	1	2
DATE OF RUN	****	04/23/03	04/23/03	04/23/03	04/23/03
CLOCK TIME: INITIAL	****	1012	1153	1012	1153
CLOCK TIME: FINAL	****	1122	1302	1122	1302
OLOGIC HAIL. I HAVE					
AVG. STACK TEMPERATURE	Degrees F	1526	1523		
AVG. SQUARE DELTA P	Inches H20	0.1414	0.1414		
NOZZLE DIAMETER	Inches	0.976	0.976		
BAROMETRIC PRESSURE	Inches HG	29.17	29.17		
SAMPLING TIME	Minutes	60	60		
SAMPLE VOLUME	Cubic Feet	68.030	65.869		
AVG. METER TEMP.	Degrees F	73.9	69.9		
AVG. DELTA H	Inches H20	4.00	4.00		
DGM CALIB. FACTOR [Y]	****	0.9876	0.9876		
WATER COLLECTED	Milliliters	138	141		
CO 2	Percent	6.46	6.08		
02	Percent	13.78	14.24		
CO	Percent				
CH4	Percent				
N 2	Percent	79.76	79.68		
STACK AREA	Square Inches	16286.0	16286.0		
STATIC PRESSURE	Inches WG.	-0.005	-0.005		
PITOT COEFFICIENT		0.84	0.84		
SAMPLE VOLUME DRY	DSCF	64.44	62.86		
WATER AT STD.	SCF	6.5	6.6		
MOISTURE	Percent	9.2	9.6		
MOLE FRACTION DRY GAS		0.91	0.90		
MOLECULAR WT.DRY	lb/lb Mole	29.59	29.54		
EXCESS AIR	Percent	189	210		
MOLECULAR WT. WET	lb/lb Mole	28.52	28.44		
STACK GAS PRESSURE	Inches HG	29.17	29.17		
STACK VELOCITY	AFPM	941	942 24633	41134	* 43527
VOLUMETRIC FLOWRATE, DRY STI	DSCFM	24687	24633 106549	41104	43021
VOLUMETRIC FLOWRATE, ACTUAL	ACFM	106465	91		
ISOKINETIC RATIO	Percent	93	91		
OALOUR ATIONS FOR CRAINLY CARIS	IC AND EMISSIO	NI DATES			
CALCULATIONS FOR GRAIN LOADIN	AG WIND EINIOOK	NA LIVITEO			
TOTAL PARTICULATE	mg	6.1	5.9	6.1	5.9
PARTICULATE CONCENTRATION	gr/dscf	0.0015	0.0014	0.0015	0.0014
PARTICULATE EMISSION RATE	lb/hr	0.31	0.31	0.51	0.54

^{*}Denotes the use of calculated flowrate based on expansion factor of LFG.

SCAQMD Method 100.1 Emission Rates

Facility: Bradley Landfill

Source: Flare #1 Job No.: W07-035 Date: 04/23/03

Run Number Load EPA F-Factor Stack Flow Rate Oxygen Carbon Dioxide	****** dscf/MMBtu dscfm %		1 as Found 10030 41134 13.78 6.46		2 as Found 10030 43527 14.24 6.08
Oxides of Nitrogen					
Concentration Concentration @ 3 % O2 Concentration Emission Rate Emission Rate	ppm ppm Ib/dscf Ib/MMBtu Ib/hr		8.5 21.3 1.03E-06 3.02E-02 2.532		7.7 20.6 9.29E-07 2.92E-02 2.427
Carbon Monoxide					
Concentration Concentration @ 3 % O2 Concentration Emission Rate Emission Rate	ppm ppm lb/dscf lb/MMBtu lb/hr	< < < < < <	20.0 50.3 1.48E-06 4.34E-02 3.642	< < < < < < < < < < < < < < < < < < <	20.0 53.7 1.48E-06 4.64E-02 3.853

Facility: Bradley Landfill

Source: Flare #1 Job No.: W07-035 Date: 04/23/03

Run No. 1

Paramete	Measured	Reference	Initial Bias	Final Bias	Average Bias	sInitial Bias	Final Bias	Average Bias	Bias Adjusted
	Conc.	Span gas	Zero	Zero	Zero	Span	Span	Span	Conc.
	(ppm,%)	(ppm.%)	(ppm.%)	(ppm.%)	(ppm.%)	(ppm.%)	(ppm.%)	(ppm.%)	(ppm.%)
NOx	8.30	10.40	0.05	0.15	0.10	10.25	10.10	10.18	8,46
NOX	0.50	10.40	0.03	0.15	0.10	10.23	10.10	10.10	0,40
02	13.68	12.01	0.03	0.00	0.01	12.00	11.85	11.93	13.78
co	10.44	50.40	0.00	0.00	0.00	50.00	49.00	49.50	10.63
000	6.20	7 00	0.00	0.00	0.04	6.00	6.00	6.04	6.46
CO2	6.38	7.00	0.00	0.02	0.01	6.92	6.90	6.91	6.46

Run No. 2

Parameter	Measured	Reference	Initial Bias	Final Bias	Average Bias	sInitial Bias	Final Bias	Average Bias	Bias Adjusted
	Conc. (ppm,%)	Span gas (ppm.%)	Zero (ppm.%)	Zero (ppm.%)	Zero (ppm.%)	Span (ppm.%)	Span (ppm.%)	Span (ppm.%)	Conc. (ppm.%)
NOx	7.54	10.40	0.15	0.15	0.15	10.10	10.25	10.18	7.67
02	14.07	12.01	0.00	0.10	0.05	11.85	11.90	11.88	14.24
со	8.76	50.40	0.00	0.00	0.00	49.00	49.80	49.40	8.94
CO2	6.05	7.00	0.02	0.02	0.02	6.90	7.02	6.96	6.08

Client: Job No.: Site: Unit:	Waste Management W07-035 Bradley Landfill Flare #1				Date: Run #: Fuel: Std. O2:	04/23/02 1 L.F.G. 3
		O2 %	CO2 %	NOx ppm	CO ppm	
Range: Span: Low:		25.00 12.01	20.00 7.00	25.00 10.40	100.00 50.40	
High:		20.90	12.01	21.00	79.20	
		** POS	ST-TEST DF	RIFT **		
Values Zero:		0.00	0.00	0.00	0.00	
Span:		11.80	7.04	10.55	50.00	
·						
Percent Drift		0.00	0.00	0.00	0.00	
Zero: Span:		0.00 -0.84	0.00 0.20	0.00 0.60	0.00 -0.40	
оран.		0.07	0.20	0.00	5.15	
	** R/	AW AVERA	GE CONCE	NTRATION	1 **	
Average:		13.68	6.38	8.30	10.44	
O2 adjust:	3.0	00	000	20.59	25.88	
Date	Time	O2 13.61	CO2 6.44	NOx 8.43	CO 0.52	
21-Apr-03	1012 1013	13.54	6.49	8.39	0.32	
21-Apr-03 21-Apr-03	1013	13.69	6.36	8.08	8.06	
21-Apr-03 21-Apr-03	1015	13.75	6.29	8.01	19.78	
21-Apr-03	1016	13.60	6.45	7.97	35.04	
21-Apr-03	1017	13.45	6.60	8.17	15.23	
21-Apr-03	1018	13.37	6.68	8.61	1.01	
21-Apr-03	1019	13.49	6.56	8.45	1.20	
21-Apr-03	1020	13.68	6.37	8.32	1.78	
21-Apr-03	1021	13.72	6.32	8.20	7.25	
21-Арг-03	1022	13.68	6.38	7.97	29.73	
21-Apr-03	1023	13.61	6.44	8.17	6.56	
21-Apr-03	1024	13.69	6.36	8.31	1.52	
21-Apr-03	1025	13.75	6.31	8.00	16.18	
21-Apr-03	1026	13.69	6.36	7.98	6.40	
21-Apr-03	1027	13.65	6.40	7.99 8.29	10.37 3.22	
21-Apr-03	1028	13.50	6.55 6.42	8.28	4.37	
21-Apr-03	1029 1030	13.62 13.94	6.42 6.09	7.51	75.95	
21-Apr-03	1030	13.94	6.34	7.31	90.98	
21-Apr-03	1032	13.70	6.52	8.23	6.62	
21-Apr-03 21-Apr-03	1032	13.65	6.41	8.19	4.09	
21-Apr-03 21-Apr-03	1034	13.69	6.36	8.29	18.56	
· · · · · · · · · · · · ·						

21-Apr-03	1035	13.79	6.27	8.10	16.65
21-Apr-03	1036	13.71	6.35	8.03	10.80
21-Apr-03	1037	13.44	6.63	8.50	4.22
21-Apr-03	1038	13.45	6.60	8.82	0.00
21-Apr-03	1039	13.61	6.43	8.71	0.95
21-Apr-03	1040	13.56	6.49	8.53	3.30
21-Арг-03	1041	13.62	6.42	8.41	2.55
21-Apr-03	1042	13.64	6.42	8.24	22.68
21-Apr-03	1052	13.71	6.32	8.63	0.49
21-Apr-03	1053	13.79	6.26	8.37	3.22
21-Apr-03	1054	13.91	6.14	8.10	3.20
21-Apr-03	1055	13.91	6.14	8.05	7.22
21-Apr-03	1056	13.82	6.22	8.07	4.52
21-Apr-03	1057	13.62	6.43	8.33	2.44
21-Apr-03	1058	13.78	6.28	8.38	2.45
21-Apr-03	1059	13.77	6.30	8.21	11.42
21-Apr-03	1100	13.59	6.49	8.33	7.27
21-Apr-03	1101	13.68	6.40	8.54	0.64
21-Apr-03	1102	13.70	6.39	8.60	0.27
21-Apr-03	1103	13.79	6.32	8.30	3.04
21-Apr-03	110 4	13.74	6.35	8.38	1.92
21-Apr-03	1105	13.89	6.21	8.29	15.19
21-Apr-03	1106	13.63	6.46	8.36	4.14
21-Apr-03	1107	13.61	6.49	8.65	0.38
21-Apr-03	1108	13.73	6.35	8.94	0.17
21-Арг-03	1109	13.85	6.24	8.23	8.99
21-Apr-03	1110	13.91	6.17	8.23	28.53
21-Apr-03	1111	13.87	6.22	8.23	14.56
21-Арг-03	1112	13.98	6.11	7.88	44.58
21-Apr-03	1113	13.60	6.49	8.07	24.21
21-Apr-03	1114	13.60	6.47	8.78	0.01
21-Apr-03	1115	13.43	6.63	8.92	0.00
21-Apr-03	1116	13.57	6.49	8.98	0.00
21-Арг-03	1117	13.79	6.27	8.56	2.60
21-Apr-03	1118	13.74	6.31	8.28	6.41
21-Apr-03	1119	13.75	6.29	8.1 9	14.21
21-Apr-03	1120	13.78	6.26	8.24	6.98
21-Apr-03	1121	13.54	6.48	8.60	1.89
21-Apr-03	1122	13.63	6.39	8.61	0.33

Client: Job No.: Site: Unit:	Waste Management W07-035 Bradley Landfill Flare #1				Date: 04/23/02 Run #: 2 Fuel: L.F.G. Std. O2: 3
		O2 %	CO2 %	NOx ppm	CO ppm
Range: Span: Low:		25.00 12.01	20.00 7.00	25.00 10.40	100.00 50.40
High:		20.90	12.01	21.00	79.20
		** POS	T-TEST DR	NFT **	
Values		0.00	0.00	0.00	0.00
Zero:		0.00	0.00 7.04	0.00 10.45	50.00
Span:		12.00	7.04	10.40	30.00
Percent Drift					
Zero:		0.00	0.00	0.00	0.00
Span:		-0.04	0.20	0.20	-0.40
	** R/	AW AVERA	GE CONCE	NTRATION	**
Average:		14.07	6.05	7.54	8.76
O2 adjust:	3.0			19.75	22.95
Date	Time	02	CO2	NOx	CO
21-Apr-03	1153	14.22	5.83	7.29	38.10
21-Apr-03	1154	13.64	6.46	7.77	22.37
21-Арг-03	1155	13.66	6.46	8.46	0.00
21-Apr-03	1156	13.94	6.18	8.37	0.00 0.51
21-Apr-03	1157	14.18	5.96 5.87	7.75 7.53	1.07
21-Apr-03	1158	14.26 14.29	5.86	7.37	4.65
21-Apr-03	1159 1200	14.25	5.69	7.30	5.06
21-Apr-03 21-Apr-03	1200	14.41	5.73	6.97	26.92
21-Apr-03 21-Apr-03	1202	14.41	5.72	7.21	15.02
21-Apr-03	1203	14.67	5.43	6.71	57.89
21-Apr-03	1204	14.25	5.89	6.38	74.60
21-Apr-03	1205	13.89	6.23	7.69	0.95
21-Арг-03	1206	13.92	6.20	7.80	0.00
21-Apr-03	1207	13.83	6.30	7.92	0.00
21-Apr-03	1208	13.87	6.26	7.93	0.00
21-Apr-03	1209	13.95	6.16	7.87	0.00
21-Apr-03	1210	14.11	6.00	7.64	0.26
21-Apr-03	1211	13.96	6.16	7.51	0.75
21-Apr-03	1212	14.24	5.87	7.62	4.65
21-Apr-03	1213	14.06	6.06	7.36	13.24
21-Apr-03	1214	14.19	5.93	7.44	5.09
21-Apr-03	1215	14.24	5.88	7.43	9.35

21-Apr-03	1216	14.33	5.80	7.05	32.59
21-Apr-03	1217	14.00	6.13	7.43	4.66
21-Apr-03	1218	14.07	6.05	7.52	1.29
21-Apr-03	1219	13.84	6.28	7.52	0.27
21-Apr-03	1220	13.69	6.42	7.88	0.00
21-Арг-03	1221	14.00	6.12	7.71	0.12
21-Apr-03	1222	14.10	6.02	7.54	0.50
21-Apr-03	1223	14.20	5.93	7.25	6.46
21-Apr-03	1232	14.34	5.75	7.01	4.97
21-Apr-03	1233	14.49	5.60	6.96	12.07
21-Apr-03	1234	14.22	5.89	6.79	30.53
21-Apr-03	1235	13.90	6.20	7.51	4.45
21-Apr-03	1236	13.95	6.16	7.63	0.00
21-Apr-03	1237	14.21	5.90	7.53	2.23
21-Apr-03	1238	13.91	6.20	7.47	1.59
21-Apr-03	1239	13.89	6.21	7.61	0.73
21-Apr-03	1240	13.82	6.28	7.85	0.00
21-Apr-03	1241	13.96	6.15	7.58	1.37
21-Apr-03	1242	13.92	6.19	7.59	0.99
21-Apr-03	1243	13.79	6.32	7.64	0.72
21-Apr-03	1244	13.87	6.24	7.67	0.19
21-Apr-03	1245	13.74	6.36	7.76	0.00
21-Apr-03	1246	13.69	6.41	8.13	0.00
21-Apr-03	1247	14.04	6.07	7.83	0.14
21-Apr-03	1248	14.13	5.99	7.36	19.52
21-Apr-03	1249	14.20	5.91	7.31	9.94
21-Apr-03	1250	13.99	6.14	7.44	7.03
21-Apr-03	1251	14.09	6.02	7.93	0.38
21-Apr-03	1252	14.15	5.97	7.55	7.15
21-Apr-03	1253	14.32	5.79	7.06	53.68
21-Apr-03	1254	14.16	5.95	7.39	15.89
21-Apr-03	1255	14.03	6.09	7.71	1.85
21-Apr-03	1256	14.25	5.86	7.75	0.94
21-Apr-03	1257	14.29	5.82	7.35	6.22
21-Apr-03	1258	14.29	5.82	7.44	12.43
21-Apr-03	1259	13.93	6.19	7.46	19.21
21-Apr-03	1300	13.85	6.28	8.27	0.00
21-Apr-03	1301	13.90	6.23	7.92	0.12
21-Apr-03	1302	13.91	6.23	7.75	2.45

And the state of t

Facility:

Bradley Landfill

Source:

Flare #1

Job No.:

W07-035

Test Date:

04/23/03

PRETEST					SYSTEM
LEAK CHECK	PASSED)			BIAS
					PreTest
	** LINEA	RITY CHE	ECK **		
RANGE:	25	20	100	25	
	02	CO2	CO	NOx	1
ZERO					NOx
Instrument	0.00	0.00	0.0	0.00	10.25
Cylinder	0.00	0.00	0.0	0.00	10.55
Difference (%)	0.00	0.00	0.0	0.00	-1.20
` ,					pass
LOW LEVEL					<u>O2</u>
Instrument	•				12.00
Cylinder					12.00
Difference (%)					0.00
					pass
MID LEVEL	40.00	0.00	50.0	40.55	<u>CO</u>
Instrument	12.00	6.96	50.0	10.55 10.40	50.0
Cylinder	12.01	7.00 -0.20	50.4 -0.4	10.40 0.60	50.0 0.0
Difference (%)	-0.04	-0.20	-0.4	0.60	pass
HIGH LEVEL					CO2
Instrument	20.50	12.00	80.0	21.00	6.92
Cylinder	20.90	12.00	79.2	21.00	6.96
Difference (%)	-1.60	-0.05	0.8	0:00	-0.20
= 111010110C (70)			-10		pass
POST TEST					Post tes
LEAK CHECK	PASSED				
	O2	CO2	CO	NOx	
ZERO					NOx
Instrument	0.00	0.00	0.0	0.00	10.25
Cylinder	0.00	0.00	0.0	0.00	10.45
Difference (%)	0.00	0.00	0.0	0.00	-0.80
					pass
LOW LEVEL	•				<u>02</u>
Instrument					11.90 12.00
Cylinder					-0.40
Difference (%)					pass
MID LEVEL					CO
Instrument	12.00	7.04	50.0	10.45	49.8
Cylinder	12.01	7.00	50.4	10.40	50.0
Difference (%)	-0.04	0.20	-0.4	0.20	-0.2
- 110101100 (70)	~1V:1				pass
HIGH LEVEL					<u>CO2</u>
Instrument	20.68	12.10	80.0	20.75	7.02
Cylinder	20.90	12.01	79.2	21.00	7.04
Difference (%)	-0.90	0.45	8.0	-1.00	-0.10
, ,					pass

Systen	n Respor	nse Time (s	seconds)
	#1	#2	#3
Upscal	e		
NOx	52	51	50
CO	54	58	52
O2	23	22	20
CO2	20	20	23
Downs	cale		
NOx	50	50	50
CO	53	55	51
O2	21	21	17
CO2	18	17	21

NO2 to NO Converter Effeciency (%)									
	cylinder	instr.	effeciency						
ppm	18.1	17.05	94.20						

Table 5-2
Trace Organic Species
Destruction Efficiency Results
Waste Management - Bradley Landfill
Flare #1
April 23, 2003

		INLET Flow rate	3531	dscfm	OUTLET Flow rate	42330.5	dscfm
Species	Conc.	Conc.	Em. Rate				
Opecies	(ppb)	(mg/dscf)	cm. nate (lb/hr)	Conc. (ppb)	Conc.	Em. Rate	Dest. Eff.
Hydrogen Sulfide	48400	1.97E+00	9.21E-01	(PPB) < 500	(mg/dscf) < 2.04E-02	(lb/hr) < 1.14E-01	(%) > 87.62
, ,			V.2.12 V.	7 000	1 2.042-02	V 1.14L-01	> 01.02
Benzene	2890	2.69E-01	1.26E-01	< 0.3	< 2.80E-05	< 1.57E-04	> 99.88
Benzychloride	< 40	< 6.07E-03	< 2.84E-03	< 0.8	< 1.21E-04	< 6.80E-04	NA
Chlorobenzene	211	2.85E-02	1.33E-02	< 0.3	< 4.05E-05	< 2.27E-04	> 98.30
Dichlorobenzenes	1480	2.60E-01	1.21E-01	< 1.1	< 1.93E-04	< 1.08E-03	> 99.11
1,1-dichloroethane	796	9.42E-02	4,40E-02	< 0.3	< 3.55E-05	< 1.99E-04	> 99.55
1.2-dichloroethane	134	1.59E-02	7.41E-03	< 0.3	< 3.55E-05	< 1.99E-04	> 97.32
1.1-dichloroethylene	162	1.88E-02	8.77E-03	< 0.3	< 3.48E-05	< 1.95E-04	> 97.78
Dichloromethane	5300	5.38E-01	2.52E-01	< 0.3	< 3.05E-05	< 1.71E-04	> 99,93
1.2-Dibromoethane	< 16	< 3.59E-03	< 1.68E-03	< 0.3	< 6.74E-05	< 3.77E-04	NA
Perchloroethene	3320	9.40E-01	4.39E-01	< 0.2	< 5.66E-05	< 3.17E-04	> 99.93
Carbon tetrachloride	< 20	< 3.68E-03	< 1.72E-03	< 0.2	< 3.68E-05	< 2.06E-04	NA
Toluene	66200	7.28E+00	3.40E+00	< 0.8	< 8.80E-05	< 4.93E-04	> 99.99
1.1.1-trichloroethane	59.2	9.41E-03	4.40E-03	< 0.2	< 3.18E-05	< 1.78E-04	> 95,95
Trichloroethene	1380	2.16E-01	1.01E-01	< 0.2	< 3.13E-05	< 1.75E-04	> 99.83
Chloroform	< 16	< 2.28E-03	< 1.06E-03	< 0.2	< 2.84E-05	< 1.59E-04	NA
Vinyl Chloride	454	3.39E-02	1.58E-02	< 0.3	< 2.24E-05	< 1.25E-04	> 99.21
m+p-xylenes	29800	3.78E+00	1.76E+00	< 0.5	< 6.33E-05	< 3.55E-04	> 99.98
o-xylene	7730	9.79E-01	4.57E-01	< 0.3	< 3.80E-05	< 2.13E-04	> 99.95
TNMHC	10187217	1.95E+02	9.10E+01	2755	5.27E-02	2.95E-01	99.68

Note: All values preceded by "<" are below the detection limit. The reported values are the detection limit. NA=Not Applicate: Destruction efficiency can not be calculated since both inlet and outlet values are below the detection limit.

APPENDIX C - Laboratory Results



Atm AA Inc.

23917 Craftsman Rd., Calabasas, CA 91302 • (818) 223-3277 • FAX (818) 223-8250

LABORATORY ANALYSIS REPORT

environmental consultants laboratory services

Organic Carbon Analysis in Water Impingers, and Methane and TGNMO Analysis in SUMMA Canister Samples from Impinger/Canister Train Sample Collection

Report Date: April 30, 2003

Client: Horizon / Waste Management

P.O. No.: Verbal

Client Project No.: W07-035

Source Location: Bradley Landfill / Sun Valley CA.

Source ID: Flare 1 outlet-

Date Received: April 23, 2003 Date Analyzed: April 25, 2003

ANALYSIS DESCRIPTION

Methane & TGNMO were measured by flame ionization detection/total combustion analysis (FID/TCA), Method 25. Organic carbon in water impinger samples were measured by Dohrman total organic carbon analyzer, water FID/TCA.

AtmAA	Sample ID	Canister Methane	Canister Ethane	Canister TGNMO	Organic Carbon as Methane	Impinger Volume	P.	lsi
		22222222222222222222222222222222		el percentación de antecesación	Mediane		F1	P ₂
04400 +0		Conc	entration in	ppmv)		(ml)		1 1
01133-18	SUMMA S12	<1	<1	2.63			592	803
0440044	Impinger H211				0.36	2.80		
01133-19	SUMMA S16	<1	<1	2.14			581	800
	Impinger H212				0.38	2.88		

TGNMO is total gaseous non-methane organics (excluding ethane), reported as ppm methane. * Note - Impinger sample results are not blank corrected. The field blank (impinger $\,$ H56) contained 0.27 ug carbon as methane, corresponding to 0.09 ppm methane for a 4.78 liter $\,$ P $_1$ and $\,$ P $_2$ are initial and final pressures measured in mm Hg.

Michael L. Porter Laboratory Director

lmninger

QUALITY ASSURANCE SUMMARY (Repeat Analyses)

Project No.: W07-035
Date Received: April 23, 2003
Date Analyzed: April 25, 2003

	Sample ID	Repeat Analysis Run #1 Run #2		Mean Conc.	% Diff. From Mean
Components	10	1	centration in p		1 TOTAL IVICAL
Methane	SUMMA S12	<1	<1		
	SUMMA S16	<1	<1		
Ethane	SUMMA S12	<1	<1		
	SUMMA S16	<1	< 1		
TGNMO	SUMMA S12	2.60	2.66	2.63	1.1
	SUMMA S16	2.10	2.17	2.14	1.6
Impinger TOC	Impinger H211	0.36	0.36	0.36	0.0
	Impinger H212	0.37	0.39	0.38	2.6

A set of 2 canister/impinger samples, laboratory numbers 01133-(18 & 19), was analyzed for methane, total gaseous non-methane organics (TGNMO), and TOC. Agreement between repeat analysis is a meaure of precision and is shown in the column "% Difference from Mean". Repeat analyses are an important part of AtmAA's quality assurance program. The average % Difference from Mean for 4 repeat measurements from the sample set of 2 canister/impinger samples is 1.4%.





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LABORATORY ANALYSIS REPORT

CO, CH₄, CO₂, TGNMO, and Ethane Analysis in Tanks and Traps by SCAQMD Method 25 (FID/TCA)

Report Date: April 29, 2003

Client: Horizon / Waste Management

P.O. No.: Verbal Client Project No.: W07-035

Source Location: Bradley Landfill / Sun Valley CA.

Source ID: Flare 1 inlet

Date Received: April 22, & 25, 2003 Date Analyzed: April 24, & 25, 2003

AtmAA	1	Sample		tank CO	tank CH ₄	tank CO ₂	tank TGNMO		tank Oxygen	P ₁	P ₂	
Lab No.		ID]	(Ca	oncentrations	s in ppmv)	1	(%)		Ī	L
•	Tank	Trap	ICV]								ı
01133-20	Α	R	Y	52.3	391000	337000	856	28700	2.69	455	800	ı
01133-21	D	0	N	54.5	390000	333000	838	29800	2.95	437	800	

trap burn system blank H

8.69

TGNMO is total gaseous non-methane organics (excluding ethane) reported as ppm methane. No ethane was found at a lower detection limit of 20 ppmv as methane.

 P_1 - Initial Pressure, mm Hg P_2 - Final Pressure, mm Hg

Michael L. Porter Laboratory Director

QUALITY ASSURANCE SUMMARY (Repeat Analyses)

Client Project No.: W07-035

Date Received: April 22, & 25, 2003 Date Analyzed: April 24, & 25, 2003

	Sample ID	Repeat Run #1	Analysis Run #2	Mean Conc.	% Diff. From Mean
Components		(Conc	entration in p		<u> </u>
со	ТК А	52.5	52.2	52.3	0.32
CH₄	ТК А	391000	390000	391000	0.08
CO ₂	ТК А	335000	339000	337000	0.51
TGNMO	тк а	841	871	856	1.8
CO ₂ in ICV (in trap, transfer tanks)	ICV Y	29200	28200	28700	1.8
		(Con	centration in	%v)	
Oxygen	TK E	2.69	2.69	2.69	0.0

A set of 2 TCA samples, laboratory numbers 01133-(20 & 21), was analyzed for CO, CH_4 , CO_2 , O2, and total gaseous non-methane organics (TGNMO). Agreement between repeat analyses is a measure of precision and is shown above in the column "% Difference from Mean". Repeat analyses are an important part of AtmAA's quality assurance program. The average % Difference from Mean for 6 repeat measurements from the sample set of 2 TCA samples is 0.74%.

Gas standards (containing CO, CH_4 , CO_2 and propane) used for TCA analyses, were prepared and certified by Praxair.





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LABORATORY ANALYSIS REPORT

environmental consultants laboratory services

SCAQMD Rule 1150.1 Components Analysis in Inlet Gas Tedlar Bag Sample

Report Date: May 1, 2003

Client: Horizon

Project Location: WMNA / Bradley LF #1

Client Project No.: W07-035 Date Received: April 23, 2003

Date Analyzed: April 23 & 24, 2003

AtmAA Lab No.:

01133-22

Sample I.D.:

W07035-F1

Components
Hydrogen sulfide

TB-IN-A (Concentration in ppmv)

48.4

(Concentration in ppbv)

	Ouncertainen in pp
Benzene	2890
Benzylchloride	<40
Chlorobenzene	211
Dichlorobenzenes*	1480
1,1-dichloroethane	796
1,2-dichloroethane	134
1,1-dichloroethylene	162
Dichloromethane	5300
1,2-dibromoethane	< 16
Perchloroethene	3320
Carbon tetrachloride	< 20
Toluene	66200
1,1,1-trichloroethane	59.2
Trichloroethene	1380
Chloroform	<16
Vinyl chloride	454
m + p-xylenes	29800
o-xylene	7730

^{*} total amount containing meta, para, and ortho isomers

Michael L. Porter Laboratory Director



Atm AA inc.

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LABORATORY ANALYSIS REPORT

Hydrogen Sulfide and Reduced Sulfur Compounds Analysis in Inlet Tedlar Bag Sample

Report Date: May 1, 2003

Client: Horizon

Project Location: WMNA / Bradley LF #1

Client Project No.: W07-035

Date Received: April 23, 2003

Date Analyzed: April 23, 2003

ANALYSIS DESCRIPTION

Hydrogen sulfide was analyzed by gas chromatography with a Hall electrolytic conductivity detector operated in the oxidative sulfur mode. All other components were measured by GC/ Mass Spec.

·	AtmAA Lab No.: Sample I.D.:	01133-22 W07035-F1 TB-IN-A
Components		(Concentration in ppmv)
Hydrogen sulfide Carbonyl sulfide Methyl mercaptan Ethyl mercaptan Dimethyl sulfide Carbon disulfide isopropyl mercaptan n-propyl mercaptan Dimethyl disulfide		48.4 0.42 3.16 <0.09 9.50 0.22 0.28 <0.06 0.22

TRS - total reduced sulfur

TRS

Michael L. Porter Laboratory Director

62.6

QUALITY ASSURANCE SUMMARY (Repeat Analyses)

Client Project No.: W07-035
Date Received: April 23, 2003
Date Analyzed: April 23 & 24, 2003

	Sample		Repeat Analysis		% Diff.
	ID	Run #1	Run #2	Conc.	From Mean
Components		(Conc	centration in	ppbv)	
Benzene	TB-IN-A	2800	2980	2890	3.1
Benzylchloride	TB-IN-A	<40	<40		
Chlorobenzene	TB-IN-A	225	197	211	6.6
Dichlorobenzenes	TB-IN-A	1530	1420	1480	3.7
1,1-dichloroethane	TB-IN-A	756	835	796	5.0
1,2-dichloroethane	TB-IN-A	142	127	134	5.6
1,1-dichloroethylene	TB-IN-A	153	170	162	5.3
Dichloromethane	TB-IN-A	5110	5480	5300	3.5
1,2-dibromoethane	TB-IN-A	<16	<16		
Perchloroethene	TB-IN-A	3180	3470	3320	4.4
Carbon tetrachloride	TB-IN-A	< 20	< 20		
Toluene	TB-IN-A	62900	69400	66200	4.9
1,1,1-trichloroethane	TB-IN-A	52.4	65.9	59.2	11
Trichloroethene	TB-IN-A	1350	1420	1380	2.5
Chloroform	TB-IN-A	<16	<16		
Vinyl chloride	TB-IN-A	363	333	454	3.3
m + p-xylenes	TB-IN-A	29800	29700	29800	0.17
o-xylene	TB-IN-A	7220	8240	7730	6.6



QUALITY ASSURANCE SUMMARY (Repeat Analyses) (continued)

·	Sample	Repeat Analysis		Mean	% Diff.
	ID	Run #1	Run #2	Conc.	From Mean
Sulfur Components		(Conc	entration in p	ppmv)	·
Hydrogen sulfide	TB-IN-A	47.7	49.2	48.4	1.5
Carbonyl sulfide	TB-IN-A	0.42	0.41	0.42	1.2
Methyl mercaptan	TB-IN-A	3.16	3.17	3.16	0.16
Ethyl mercaptan	TB-IN-A	< 0.09	<0.09		
Dimethyl sulfide	TB-IN-A	9.54	9.47	9.50	0.37
Carbon disulfide	TB-IN-A	0.22	0.21	0.22	2.3
iso-propyl mercaptan	TB-IN-A	0.27	0.28	0.28	1.8
n-propy! mercaptan	TB-IN-A	<0.06	<0.06		
Dimethyl disulfide	TB-IN-A	0.24	0.20	0.22	9.1

One Tedlar bag sample, laboratory number 01133-22, was analyzed for SCAQMD Rule 1150.1 components, hydrogen sulfide, and total reduced sulfur compounds. Agreement between repeat analyses is a measure of precision and is shown above in the column "% Difference from Mean". Repeat analyses are an important part of AtmAA's quality assurance program. The average % Difference from Mean for 21 repeat measurements from the one Tedlar bag sample is 3.9%.





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LABORATORY ANALYSIS REPORT

environmental consultants laboratory services

SCAQMD Rule 1150.1 Components Analysis in Outlet Tedlar Bag Sample

Report Date: May 1, 2003

Client: Horizon

Project Location: WMNA / Bradley LF #1

Client Project No.: W07-035 Date Received: April 23, 2003 Date Analyzed: April 23 & 24, 2003

AtmAA Lab No.:

01133-23

Sample I.D.:

W07035-F3

TB-OUT-A

(Concentration in ppbv) Components

Hydrogen sulfide	< 500
Benzene	< 0.3
Benzylchloride	<0.8
Chlorobenzene	< 0.3
Dichlorobenzenes*	< 1.1
1,1-dichloroethane	< 0.3
1,2-dichloroethane	< 0.3
1,1-dichloroethylene	< 0.3
Dichloromethane	< 0.3
1,2-dibromoethane	< 0.3
Perchloroethene	< 0.2
Carbon tetrachloride	< 0.2
Toluene	< 0.8
1,1,1-trichloroethane	< 0.2
Trichloroethene	< 0.2
Chloroform	< 0.2
Vinyl chloride	< 0.3
m + p-xylenes	< 0.5
o-xylene	< 0.3
O-Aylene	\0.0

^{*} total amount containing meta, para, and ortho isomers

Michael L. Porter Laboratory Director Source: Flare 1 Job No.: W07-035 Test Date: 04/21-23/03

DATA SHEET FOR PARTICULATE MATTER SCAQMD METHOD 5.1

DATE SAMPLED: 04/21-23/03

DATE EXTRACTED: 04/22-24/03

RUN #1

DATE EXTRACTED: 04/22-24/0	3					
	SAMPLE ID	BEAKER/ FILTER ID	VOLUME	INITIAL	FINAL	NET WEIGHT(g)
A - FILTER CATCH FILTER ACID FILTER SULFATE	W07035-5.1-F1-PF-1	G00200	NA	0.0833	0.0836	0.0003 0.0000
B - PROBE CATCH PROBE ACID PROBE SULFATE						0.0000 0.0000
PROBE SULFATE						0.0000
C - IMP.CATCH(INSOL) INSOLUBLE ACID INSOLUBLE SULFATE	W07035-5.1-F1-EF-1	G03028	620	0.0817	0.0825	0.0008 0.0000 0.0000
D - IMP. CATCH (SOL) SOLUBLE ACID SOLUBLE SULFATE	W07035-5.1-F1-DI-1	030034	620	29.3473	29.3523	0.0050 0.0000 0.0000
E - ORGANIC EXTRACT	W07035-5.1-F1-MC-1	030047	125	30.5883	30.5882	0.0000
TOTAL PARTICULATE	(A+B+C+D+E)					0.0061
SOLID PARTICULATE	(A+B+C+D)					0.0061

Source: Flare 1 Job No.: W07-035 Test Date: 04/21-23/03

DATA SHEET FOR PARTICULATE MATTER SCAQMD METHOD 5.1

DATE SAMPLED: 04/21-23/03 DATE EXTRACTED: 04/22-24/03 RUN #2

DATE EXTRACTED: 04/22-24/03						1
	SAMPLE ID	BEAKER/ FILTER ID	VOLUME	INITIAL	FINAL	NET WEIGHT(g)
A - FILTER CATCH FILTER ACID FILTER SULFATE	W07035-5.1-F1-PF-2	G00198	NA	0.0845	0.0851	0.0006 0.0000
B - PROBE CATCH PROBE ACID						0.0000 0.0000
PROBE SULFATE						0.0000
C - IMP.CATCH(INSOL) INSOLUBLE ACID	W07035-5.1-F1-EF-2	G03029	556	0.0820	0.0833	0.0013 0.0000
INSOLUBLE SULFATE						0.0000
D - IMP. CATCH (SOL) SOLUBLE ACID SOLUBLE SULFATE	W07035-5.1-F1-DI-2	030036	556	30.3478	30.3518	0.0040 0.0000 0.0000
E - ORGANIC EXTRACT	W07035-5.1-F1-MC-2	030041	125	30.5197	30.5196	0.0000
						Kennyagan and d
TOTAL PARTICULATE	(A+B+C+D+E)					0.0059
SOLID PARTICULATE	(A+B+C+D)					0.0059

Facility: Waste Management/Bradley

SCAQMD Method 5.1

Source: Flare 1 Job No.: W07-035 Test Date: 04/21-23/03

DATA SHEET FOR PARTICULATE MATTER SCAQMD METHOD 5.1

DATE SAMPLED: 04/21-23/03

BLANK

DATE EXTRACTED: 04/22-24/	03					
	SAMPLE ID	BEAKER/ FILTER ID	VOLUME	INITIAL	FINAL	NET WEIGHT(g)
A - FILTER CATCH FILTER ACID FILTER SULFATE	PF-BLANK	G003021	NA	0.0846	0.0845	0.0000 0.0000
B - PROBE CATCH PROBE ACID						0.0000 0.0000
PROBE SULFATE						0.0000
C - IMP.CATCH(INSOŁ) INSOLUBLE ACID INSOLUBLE SULFATE	EF-BLANK	G03023	1000	0.0856	0.0852	0.0000 0.0000 0.0000
D - IMP. CATCH (SOL) SOLUBLE ACID SOLUBLE SULFATE	DI-BLANK	030024	1000	29.3816	29.3816	0.0000 0.0000 0.0000
E - ORGANIC EXTRACT	MC-BLANK	030027	125	30.4833	30.4830	0.0000
TOTAL PARTICULATE	(A+B+C+D+E)					0.0000
SOLID PARTICULATE	(A+B+C+D)					0.0000

CHAIN OF CUSTODY RECORD

	Client/Project Name Project Local	ation	TODI NE	/ /	
	1.	VALLEY	, CA	ANALYSES	
:	Project No. Field Logbook			6//////	
	W07. 035				
	Sampler: (Signature) Chain of Custody	y Tape No.			
	03:				
		<u> </u>			
	Sample No./ Lab Sample Identification Date Time Number	Type Sam		/ REMARKS	
W	7.035.5.1-F1-PF1 U2-24.03				
	-0/1				
	PF2				
	D/2 ₩				
		, , , , , , , , , , , , , , , , , , ,			
		W-17-3	 .		
	Relinquished by: (Signature)	Date	Time	Received by: (Signature) Date Time	
		04.24.03	1		Ó
	Relinquished by: (Signature)	Date	Time	Received by: (Signature) Date Time	
				7	
	Relinquished by: (Signature)	Date	Time	Received for Laboratory: (Signature) Date Time	
	Sample Disposal Method:	Disposed of	of by: (Signa	Innature) Date Time	_
ı					ı
	SAMPLE COLLECTOR	ANALYTICA	AL LABORA	RATORY	
	HORIZON AIR MEASUREMENT SERVICES, INC			·	ļ
Ì	996 Lawrence Drive, Suite 108				
	Newbury Park, CA 91320 (805) 498-8781 Fax (805) 498-3173			N º 7780	

APPENDIX D - Field Data Sheets

Facility: Source: Job #: Date: Operator	4/23	# / <u>Fnlo</u> r Sta - 03 < Pite - /03 - Pite	ro. Press: tic Press: ot Tube #: ot Tube Type: gnahelic:	2 9.17 + 10.0 18'5tc1 5+01	D ₁ upstream: D ₁ downstream: Stack Diameter: Leak Cl	6.6 8.7 13.25 heck Final:
Run #:	1,2					1/0
Point #	Position in.	/ Velocity Head in. H₂O.		Cyclonic Flow	Side V	iew
A6	/2.7	1.0 1.1	141 143			····
5	17.3	1.3 1.4	141 143	3		
4	9.3	1.2 1.3	141 143			
3	3 .9	1.2 1.1	141 143			
_ 2	1-9	1.1 1.1	141 143			
/	0.6	1.0 1.0	141 143		1687"-16	~ 115''_ >
B 6		1.01.0	14/ 14/3		1	
5		1.1 1.0	14) 143			
4		1.1 1.2	141 143			
3			141 143 141 143			
2		1.) 1.)	141 143		Top Vi	ew
. ,						
	<u> </u>	<u> </u>				
		<u></u>			The state of the s	
					BE)
						
Average		√ΔP= ,	T _s = /	_=		
orizon Air	/. 0 Measurement S	559/1.0593 68 ervices, Inc.58	41.0 43. 58 56 FORMS VELOCK		1	

PLANT Brack of LF DATE 4-23-03 LOCATION Sup Vally CY OPERATOR 18 TV SOURCE Flav + Inter RUN NO. MU. 1 SAMPLE BOXNO. C7 METER BOX NO. ASSUMED MOISTURE, %_ METER ΔH@ 1.650 --Y= 0.9873 PROBE I.D. NO. — NOZZLE DIAMETER, in. ___ STACK DIAMETER, in. PROBE HEATER SETTING -PRE TEST LEAK CHECKS METER 2.005 @ 15 in. Hg PITOTS _ @ in. Hg HEATER BOX SETTING TIME START 10:12 Δ Cp FACTOR_ ORSAT_ FILTER NO. T_{m IN} °F T_OUT OVEN IMP. ΔΡ √∆P ΔΗ Vm VAC. TIME P# T_{s} OUT °F in H₂O in H₂O ٩F (in Hg) 7~ 76 132 6-4-m - 10°− 7--00 561.557 50 5145/v 2 569.9 10 1.7 74 72 53 2 20 ଞା 2 1.7 74 577.1 53 30 1.7 585-2 53 2 **%**₹ 7.5 40 90 J 1.7 78 55 2 30 1.7 600.4. 93 56 B 60 56-608.402 46.845 78.8 1112 TIME END = Meter Lows POST TEST LEAK CHECKS Impinger Volume Silica Gel Volume of Liquid Wght. Pitots V A in. Hg Water Collected Orsat NA 277 124 104 2 Final Orsat Meas. Time CO, 0, CO N₂ 100 0 CC257 Initial 24 2 6 20 Liquid Collected Total Vol. Collected D, Nozzle Cal D, D_{i} Average HORIZON AIR MEASUREMENT SERVICES, INC. 055

PARTICULATE FIELD DATA

Bradley LF метек вох no. <u>5</u> метек дн <u>@ 1. С бът</u> у= <u>6 9 б 7 3</u> Probe i.d. no. <u>-</u> ASSUMED MOISTURE, % AMBIENT TEMPERATURE 65 BARO. PRESS. LOCATION STATIC PRESS. 59. TW OPERATOR_ NOMAGRAPH INDEX Flavet NOZZLE DIAMETER, in. -SOURCE Inler STACK DIAMETER, in. M4.) RUN NO. PRE TEST LEAK CHECKS
METER 2.05 @ 15 in. Hg PROBE HEATER SETTING -SAMPLE BOX NO. HEATER BOX SETTING_ TIME START /153 PITOTS in. Hg @__ Δ Cp FACTOR_ ORSAT FILTER NO. T_m OUT OVEN IMP. VAC. ٧m T_{mN} √∆P ΔH ΔΡ TIME Ρ# T_{s} OUT °F (in Hg) °F in H₂O ٩F in H₂O 52 3 හිථ ١٦ 610.958 00 2 91 53 81 618.6 10 1.7 626.3 93 25 Q. ヽヲ 82 20 <u>94</u> 634.1 82 S 2 1.7 70 <u> 94</u> 2 641.5 52 E8 1.7 40 94 2 649.7 € ≥ 57 1.7 50 657.773 60 🧢 १४९८ 86. 4 46.815 1.70 Avg. TIME END = POST TEST LEAK CHECKS Sitica Gel Impinger Volume Meter_ L. 205 in. Hg @ 15 Wght. Volume of Liquid Pitots____ in. Hg Water Collected Orsat --3 140 CO N_2 104 Orsat Meas. Time CO₂ O₂ Final 100 100 Initial 3 18 40 Liquid Collected Total Vol. Collected Average D, $\mathbf{D}_{\mathbf{i}}$ Nozzle Cal D, HORIZON AIR MEASUREMENT SERVICES, INC. 056

PARTICULATE FIELD DATA

PARTICULATE FIELD DATA

METERSON BOOK	PLANT B	radley LE
E #	DATE	4-23-03
	LOCATION	Sun Valley, CA
70	OPERATOR	50, TW , C54
Communication of	SOURCE F	lave#1' OUTLE
ı	RUN NO.	M5.1
	SAMPLE BOX!	10. C 3

TIME START 1012

METER BOX NO. 4
METER ΔH@ 1.7693
Y= 0.9876
PROBE I.D. NO. /0-2
NOZZLE DIAMETER, in. 9.976
STACK DIAMETER, in. 1947
PROBE HEATER SETTING
HEATER BOX SETTING
Δ Cp FACTOR O. 84
FILTER NO. 600 200

ASSUMED MOISTURE, % /2
AMBIENT TEMPERATURE 65 F
BARO, PRESS. 22.12
STATIC PRESS. - Q.005
NOMAGRAPH INDEX 200

	P#	TIME	Т _s °F	ΔP in H ₂ O	√∆F	•	ΔH in H ₂ O	Vm ft ¹	T _{m N} °F	T _m OUT	OVEN °F	IMP. OUT °F	VAC. (in Hg)
	A 12	0,0	1517	0.02	7		4.₽	424.885	6+ } e	6170	T	5 3.	Z7
cassanda	11	2.5	157>	0 02			4.0	427.5	80₹	7470		F54-54	
	10	5.0	1500	0.02		·	4.0	430.4		71		54	7
	9	7.5	1525	0.02		-	4.0	433 7	73	71		56	7
	8	120	1523	ე ე			4.0	436.1	73	71		56	7
	7	12.5	(518	0-02			4.0	438.9	74	71		52	7
	6	15.0	1517	D.07			4,0	441.7	74	72		56	3
İ	5	17.5	1515	0.02			4.0	444.6	75	72		57	7
	4	220	1512	0.0			4.0	447.4	75	72		57	7
	3	22.5	1551	6.02			LIJO	430.3	75	72		5%	7
	2	25.0	1554	0.02			4.0	453.2	76	93		56	7
)	225	1530	0.02			4.0	455.9	76	74		57	7
	B 12	30,0	1545	0.02	Poorch	يومص	૫.૦	458.660	75	72		54	7
	37	32.5	1526	0.02			4.0	467.8	76	73		55	ラム
	10	35.0	1515	0.02			4.0	464.4	76	74		56	77
	9	325	1524	0.02			4.0	467.3	76	74		8.	マ
ļ	8	420	1532	0 - 0 2			4.0	470.1	77	74		56	3
-	7	42.5	1520	0.02			4.0	473.2	77	74		57	7
	5	45.0	1543	0.02			4.0	44	37	74		57	7
-	5	47.5	1532	0.ఎఓ			4.0	478.7	77	74		57	7
- 1	4	52.0	1520	0.62			4.0	481.5	77	74		59	7
	3	52.5	1518	0.0Z			4,0	484.3	77	74		57	7
	2	55.0	1523	6,02			4.0	467.2	77	ં ગ્ય		57	7
	/	57.5	1515	6.02	1		٧.0	490.3	77	75		56	7
		63.0					<i>-</i>	492.915			4		
	Avg.		1525.8		0.1414		4.0	68.030	73.				
;	IME END	= //-			50	3	58	53	53				

Volume of Liquid		Impinge	Silica Gel Wght.		
Water Collected	1	2	3	4	4
Final	184	127	9		274
Initial	100	آ ق	0		256
Liquid Collected	84	27	4		18
Total Vol. Collected					138

Meter 1.005 @ 15 in. Hg
Pitots @ 15 in. Hg
Orsat

Orsat Meas.	Time	CO ₂	O ₂	со	N ₂
1					
2					
, 3					
Nozzle Cal	D,	D,	D_1	Ave	erage
	0.976	0.975	0.976	0,9	76

SB

HORIZON AIR MEASUREMENT SERVICES, INC.

PARTICULATE FIELD DATA

PLANT Bradley LF
DATE 4-23-03
LOCATION SUN VALLEY CA
OPERATOR 58 TW. C3M
SOURCE FISION*/ OUTLOT
RUN NO. 2 M.5.1
SAMPLE BOX NO <i>C//</i>

PROBE I.D. NO. NOZZLE DIAMETER, in. STACK DIAMETER, in. PROBE HEATER SETTING HEATER BOX SETTING

ASSUMED MOISTURE, % AMBIENT TEMPERATURE 65 BARO, PRESS, STATIC PRESS NOMAGRAPH INDEX

Δ Cp FACTOR FILTER NO.

METER ΔH@ 1- 76 Y= 0.9676

METER BOX NO.

PRE TEST LEAK CHECKS
METER 2.005 @ 15 in. Hg
PITOTS @ 4" in. Hg in. Hg ORSAT

TIME START 1153

P#	TIME	T _s ℉	ΔP in H ₂ O	√∆P	ΔH in H₂O	Vm ñ¹ 497.33⊋∓	T _{mw} °F	T _m OUT °F	OVEN °F	IMP. OUT 'F	VAC (in Hg
A 12	0.0	1541	0.02	4	4.0.	/ (4) 7 / 1 / 1	66	66	7	53	7 1
11	2.5	1511	0.02		4.0	499-6	67	66		53	7
12	5.0	1509	0.02		4.0	502.3	68	46		54	7
9	2.5	1417	0.02		4.0	505.2	69	68 66"		54	7
8	12,0	1513	0.02		4,0	567.9	70	67		54	7
2	12.5	1526	6.02		4.0	510.6	ř	67		54	7
6	15.0	1526	0.02	<u> </u>	4.0	513.60	71	68		55	7
5	12.5	1531	0.02		4.0	516.1	71	હુજ		5%	7.
4	20.0	1540	0.02		٧,٠٥	518.7	71	68		56	_ ک
3	22.5	1522	0.02		4.0	521.4	72	७९		57	7
2	250	1515	6.02		4.0	524.2	72	69		53	7
7	27.5	1516	0.02		4.0	526.8	72	69		57	7 ,
B 12	300	1539	0.02		4.0	529.563	70	67		54	7
17	32.5	1552	0.02		4.0	537.4	7	७४		54	7
19	35.0	1540	0.02		4.0	535.2	71	68		56	·7·1
9	37.5	1539	0.02		4.0	537.9	ትշ	68		56	ጉ
8	430	1524	0.02	1	4.0	540,8	72_	७५		52	7
7		1509	0.02		4.0	543.6	ठेठ	70		56	7
	7.7	1504	0.02		4.0	546.2	7-3	रेठ		5%	7
5		1515	0.02		4.0	249.5	75	70		57	7
7		1524	0.02		4.0	551.9	74	7(< <u>4</u>	7_1
3		1500	0.02		4.0	554.7	74	7-1		57	7
2	55.3	1522	0.02		4.0	557.6	74	71.		27	7
/	57.5	1514	602		4.0	560.3	74	71		56	7
	60.0			V	4	563.246			Y		- ing
		1527 I	1	0.1414	40	65.869	69	9			

5B

Volume of Liquid		Impinge	Silica Gel Wght.		
Water Collected	11	2	3	4	5
Final	187	124	9		289
Initial	/20	100	0		268
Liquid Collected	87	24	9		21.0
Total Vol. Collected					141

Meter in. Hg Pitots_ in. Hg @ Orsat 1/4

38 .

Orsat Meas.	Time	CO,	0,	со	N ₂
1		·			
2					
3					En-
Nozzle Cal	D _i	D,	D ₁	Ave	rage
-	0.976	0.975	0.9%	0.970	5

58

TIME END =

SCAQMD METHOD 25 FIELD SAMPLING DATA SHEET

Control Device: FLMe 井 1
Sample Location: INCET
Ambient Temp.: 45°
Baro. Pressure: 29.17

4	SAMPLE A		
Tank #:	Tı	rap #:	
Initial Vacuum: _	2.5	Tory /30'	7
Final Vacuum: 🔼	, "		
Start Time: 10:11	ב		

В
p#:
11/3011

TIME (min.)	VACUUM ("Hg)	FLOW (cc/min)
00	30	~/5v
05	25 1/2	
10	27	
15	251/2	
20	24	
25	72 1/2	
30	21	
35	1	
40	191/2	
45	161/2	
50	15	
55	131/2	
60		~150

TIME (min.)	VACUUM ("Hg)	FLOW (cc/min)
00	30	~150
05	281/2	
10	2.7	
15	251,	
20	24	
25	221/2	
30	21	
35	7 2042/5/2	
40	18	
45	161/2	
50	15	
55		
60	13½ 12	~ 150

LEAK RATE	
Pre Test :	\/\/\/\/\/\/\/\/\/\/\/\/\/\/\/\/\/\/\/
Post Test:	V / ~

059

SCAQMD METHOD 25 FIELD SAMPLING DATA SHEET

Job #: <u>(NO7 - 035</u>
Facility: Brodey LANGII
Location: Sun VAILEY, CA
Date: 4-23-03
Operator: CSM, TW, SB

Control Device: 🖄	lare#1
Sample Location:	OUTLET
Ambient Temp.: _	650
Baro. Pressure:	

SAMPLE A

Tank #: 51 1	<u> </u>	Frap #: _	<u> 17 J-11</u>
Initial Vacuum:	3.8 1	DVY	
Final Vacuum: _	6 in	Hu	
Start Time:	10:14	7	

	SAMPLE B
Tank #: 5 16	
Initial Vacuum: _	3,8 TOVV
Final Vacuum: _	6 in Ita
End Time:	11:14

TIME (min.)	VACUUM ("Hg)	FLOW (cc/min)
00	30	567
05	3-8	
10	26	
15	24	
20	22	
25	2-0	
30	18	
35	16	
40	14	
45	12	
50	16	
55	8	
60	6	

TIME (min.)	VACUUM ("Hg)	FLOW (cc/min)
00	30	567
05	28	
10	26	
15	24	
20	22	
25	20	
30	18	
35	/6	
40	14	
45	12	
50	10	
55	8	
60	6	\//

Pre Test : Post Test:

HORIZON AIR MEASUREMENT SERVICES, INC.

000

INTEGRATED BAG SAMPLING DATA FORM

, Run Numbe	er:
Date: 4/23/03	Plant: BRADLEY LANDFILL
Sampling Location: FLARE #	1 OUTLET
Barometric Pressure: 22.17	
Ambient Temp. ♥: _ \$5°F	Stack Temp. 名: 16つつ 午
Operator: C5M	

Star 1012		A	В		
Time	Traverse Point		eter Flow , cm³/min.		% Dev.ª
၅၁	5145/c	67	167	0	
10		67	67	0	
20		67	67	O	
30		67	67	0	
40		67	67	0	
50		67	67	0	· · · · · · · · · · · · · · · · · · ·
60		67	67	0	
			· 		
	, <u>wa</u>		···· <u>-</u>		
					
		<u></u>			
		Av	g. =		

% Dev. =
$$(\frac{Q - Q_{avg}}{Q_{avg}})$$
 100; must be $\leq 10\%$

H:\WPDOCS\FORMS\Integrated Bag Sampling Form.wpd

CEM TEMPERATURE DATA

Facility: BRADLEY LANDFILL

Job No.: WO 7 - 035
Source: FLARE #1

Probe Temp Settings: >250 C Heated Line Temp Settings: > 250 F

		Т	TEMPERATURES OF											
	Time	Condenser Outlet	Probe	Teflon Line										
1	R1 00	35	>250	> 250										
2	10	35												
3	20	36												
4	30	35												
5	40	35												
6	50	35 35												
7	60	35												
8	RZ 00	35												
9	10	32												
10	20	3.5	/											
11	3-	35												
12	40	35												
13	20 30 40 50	35	1											
14	60	35	<u> </u>	-										
15														

SAMPLE TRAIN REQUEST/CHAIN OF CUSTODY FORM SCAQMD Method 4, 5, 6, 12 Multiple Metals, Semi Volatiles, Acids

Method(s):	7.035	F. /Wacte Manage	No. Trains/Method: 2 Source Test Date: 04.23.03 Date Needed: 04.22.03 Prepared by:								
PROBE ID	JUMPER ID	IMPINGERS TRAIN ID	FILTER HOLDER ID	RUN #	SOURCE ID						
	<u>C3</u> <u>CII</u>	C3 CII	C3 (G00200) C11 (G00198)	2							
Relinquished Relinquished Relinquished Relinquished	to: 3 to: by: by: by: by: by: by: by: by: by: by	1/2-	Date: 4/23/ Date: 4/23/ Date: 4/23/ Date: 4/23/ Date: 5/24/ Date: 5/24/ Date: 5/24/ Date: 5/24/ Date: 5/24/	103 103 703	Time:						
Sample Trains	Received Inta		Date: <u></u>								

APPENDIX E - Calibration Information



5700 South Alameda Street Los Angeles, CA 90058 Telephone: (323) 585-2154 Facsimile: (714)542-6689

CERTIFICATE OF ANALYSIS

CUSTOMER HORIZON AIR MEASUREMENTS DATE

11/21/02

P.O NUMBER

8557

REF. NUMBER

73184900

REQUESTED COMPOSITION

GAS

CONCENTRATION

NITROGEN DIOXIDE (AS NOX)

19 ppm

ATR

BALANCE

ANALYTICAL ACCURACY

±2 %

ANALYTICAL METHOD

INSTRUMENT

ANALYTICAL PRINCIPLE

Thermo Env. 42H S/N 42H-44979-273

Chemiluminescence

Thermo Env. 42H S/N 42H-44979-273

Chemiluminescence

VALUES NOT VALID BELOW 150 PSIG.

SRM UNCERTAINTY ± 2 %

NOX CONC. LAST CERTIFIED ON 10-19-02 WAS 17.9 ppm.

THIS CYLINDER NO.

SA 15361

CERTIFIED CONCENTRATION

CYLINDER PRESSURE

1250 **PSIG**

NITROGEN DIOXIDE (AS NOX)

18.1 ppm

EXPIRATION DATE

05-21-03

BALANCE

CLASSIFICATION

PRIMARY STANDARD

ANALYTICAL ACCURACY

±2 %

BATCH NUMBER

N/A

0.4 ppm

LOT NUMBER

PART NUMBER

109210507

EV AINX19MP-AS

CYLINDER SIZE AS CGA 660

CFT 85

ANALYZED BY

PHU TIEN NGUYEN

CERTIFIED BY

IMPORTANT

Information contained herein has been prepared at your request by qualified experts within Praxair Distribution, Inc. White we believe that the information is accurate within the limits of the analytical methods employed and is complete to the extent of the specific analyses performed, we make no warranty or representation as to the suitability of the use of the information for any particular purpose. The information is offered with the understanding that any use of the information is at the sole discretion and risk of the user. In no event shall the liability of Praxair Distribution, Inc., arising out of the use of the information contained herein exceed the fee established for providing such information.

065



5700 South Alameda Street Los Angeles, CA 90058 Telephone: (323) 585-2154

Facsimile: (714)542-6689

CERTIFICATE OF ANALYSIS / EPA PROTOCOL GAS

CUSTOMER

HORIZON AIR

P.O NUMBER

REFERENCE STANDARD

COMPONENT

NIST SRM NO.

CYLINDER NO.

CONCENTRATION

NITRIC OXIDE GMIS

vs.SRM#2629

SA 18096

12.7 ppm

ANALYZER READINGS

R=REFERENCE STANDARD

Z = ZERO GAS

C=GAS CANDIDATE

1. COMPONENT	NITRI	C OXIDE	GMIS		ANALYZ	ER MAKE-MO	DDEL-S/N T		S/N 42H-44979			\$10.59 50.59
ANALYTICAL	PRINC	CIPLE	Chen	nilumine	scence			LAST CALIBR	ATION DATE	09/09/	02	1792
FIRST ANALY	SIS DA	TE	09/0	05/02				SECOND ANAI	LYSIS DATE	09/13/	02	
Z -0.04	R	15.58	C	12.59	CONC.	10.27	Z -0.03	R 16.90	C 13.57	CONC.	10.20	E.
R 15.62	Z	-0.04	C	12.58	CONC.	10.23	R 16.88	${f Z}$ -0.03	C 13.50	CONC.		Mary Mary
Z -0.04	C	12.65	R	15.72	CONC.	10.23	$\mathbf{Z}_{-0.03}$	C 13.57	R 16.85	CONC.	10.23	益
U/M ppm			N	ÆAN TE	ST ASSAY	10.24 ppm	U/M ppm		MEAN TES	ST ASSAY	10.20	mqq

NOx values for reference only. All values not valid below 150 psig.

THIS CYLINDER NO.

CC 150046

EPA-600/R97/121

CERTIFIED CONCENTRATION

HAS BEEN CERTIFIED ACCORDING TO SECTION OF TRACEABILITY PROTOCOL NO. Rev. 9/97

NITRIC OXIDE

10.2 ppm

NITROGEN

NOx

BALANCE 10.4 ppm

PROCEDURE

CERTIFIED ACCURACY

% NIST TRACEABLE

CYLINDER PRESSURE

2000 PSIG

CERTIFICATION DATE

09/13/02

EXPIRATION DATE

09/13/04

± 1

TERM 24 MONTHS

ANALYZED BY

PHU TIEN NGUYEN

CERTIFIED BY

IMPORTANT

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MINAMIN

rraxair 5700 South Alameda Street

Los Angeles, CA 90058 Telephone: (323) 585-2154 Facsimile: (714) 542-6689

CERTIFICATE OF ANALYSIS / EPA PROTOCOL GAS

CUSTOMER

HORIZON AIR

P.O NUMBER

REFERENCE STANDARD

COMPONENT

NIST SRM NO.

CYLINDER NO.

CONCENTRATION

NITRIC OXIDE GMIS

vs.SRM#1683

CC 95448

22.4 ppm

ANALYZER READINGS

R=REFERENCE STANDARD

Z=ZERO GAS

C=GAS CANDIDATE

1.	COMPONENT	NITRIC OXIDE	GMIS	ANALYZ	ER MAKI	E-MOI	DEL-S/N	Thermo Env. 42H	S/N 42H-44979	-273	
	ANALYTICAL	PRINCIPLE	Chemiluminesc	ence				LAST CALIBR		08/09/	02
	FIRST ANALY	SIS DATE	08-20-02					SECOND ANAI	YSIS DATE	08-27-6	-
	Z 0	R 22.6	C 21.0	CONC.	20.8	:	Z 0.0	R 22.66	C 21.02	CONC.	20.8
	R 22.5	Z 0	C 21.0	CONC.	20.9		R 22.65	Z 0.0	C 21.03	CONC.	
	Z 0	C 21.1	R 22.7	CONC.	20.8		Z 0.0	C 21.03	R 22.67	CONC.	
	U/M ppm		MEAN TEST	ASSAY	20.8		U/M ppm	n	MEAN TES		

NOx values for reference only.
All values not valid below 150 psig.

THIS CYLINDER NO. SA 7833 HAS BEEN CERTIFIED ACCORDING TO SECTION EPA-600/R97/121 OF TRACEABILITY PROTOCOL NO. Rev. 9/97 **PROCEDURE** CERTIFIED ACCURACY ± 1 % NIST TRACEABLE CYLINDER PRESSURE 2000 PSIG CERTIFICATION DATE 08/27/02 EXPIRATION DATE 08/27/04 TERM 24 MONTHS

ANALYZED BY

PHU TIEN NGUYEN

CERTIFIED BY

NITRIC OXIDE

NITROGEN

NOx

MICHAEL TSANG

20.8 1ppm

BALANCE

21.0 ppm

CERTIFIED CONCENTRATION

IMPORTANT

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Facsimile: (714)542-6689

CERTIFICATE OF ANALYSIS / EPA PROTOCOL GAS

CUSTOMER

HORIZON AIR

P.O NUMBER

REFERENCE STANDARD

COMPONENT

NIST SRM NO.

CYLINDER NO.

CONCENTRATION

CARBON MONOXIDE GMIS NITRIC OXIDE GMIS

vs.SRM#1689 vsSRM#1683b

SA 18494 SA 10788 50.0 ppm 48.61 ppm

ANALYZER READINGS

R=REFERENCE STANDARD

Z=ZERO GAS

C=GAS CANDIDATE

 COMPONENT 	CARBON MONOXII	DE GMIS A	ANALYZ	ER MAKE-MOI	DEL-S/N s	Siemens Ultramat	5E S/N A12-7	29	•
ANALYTICAL	PRINCIPLE	NDIR				LAST CALIBRA	ATION DATE	11/14/0	2
FIRST ANALYS	SIS DATE	07/23/02				SECOND ANAL	YSIS DATE	11/21/0	2
Z 0.0	R 50.6	C 50.3	CONC.	50.3	Z 0.0	R 50.0	C 50.6	CONC.	50.6 f
R 50.6	Z 0.0	C 50.3	CONC.	50.3	R 50.0	Z 0.0	C 50.6	CONC.	50.6
Z 0.0	C 50.3	R 50.6	CONC.	50.3	$\mathbf{Z}_{0.0}$	C 50.6	R 50.0	CONC.	50.6
U/M ppm		MEAN TEST	ASSAY	50.3 ppm	U/M ppm		MEAN TES	T ASSAY	50.6 ppm
2. COMPONENT	NITRIC OXIDE	GMIS A	ANALYZ	ER MAKE-MOI	DEL-S/N g	Beckman 951A S	/N 0101354		1
ANALYTICAL	PRINCIPLE	Chemiluminescer	nce			LAST CALIBRA	ATION DATE	11/08/0	2
FIRST ANALY	SIS DATE	07/23/02 .		:		SECOND ANAL	YSIS DATE	11/21/0	2
Z 0.0	R 429.0	C 417.2	CONC.	50.2	Z 0.0	R 428.0	C 438.3	CONC.	49.8
R 427.9	Z 0.0	C 416.7	CONC.	50.2	R 427.6	Z 0.0	C 437.9	CONC.	49.8
Z 0.0	C 416.0	R 429.8	CONC.	49.9	Z 0.0	C 436.6	R 426.5	CONC.	49.8
U/M mv		MEAN TEST	ASSAY	50.1	U/M mV		MEAN TES	T ASSAY	49.8 ppm -

Values not valid below 150 psig.

NOx values for reference use only.

FIRST ANALYSIS OF CO USED GMIS# SA 17996 & NO USED NO GMIS# SA 13019.

THIS CYLINDER NO.

SA 8852

CERTIFIED CONCENTRATION

HAS BEEN CERTIFIED ACCORDING TO SECTION

EPA-600/R97/121

CARBON MONOXIDE 50.4 ppm

OF TRACEABILITY PROTOCOL NO.

Rev. 9/97

NITRIC OXIDE 50.0 ppm

PROCEDURE

CERTIFIED ACCURACY

NITROGEN

BALANCE

% NIST TRACEABLE

NOx

50.1 ppm

CYLINDER PRESSURE

± 1

CERTIFICATION DATE

2000 PSIG

11/21/02

EXPIRATION DATE

11/21/04

TERM 24 MONTHS

ANALYZED BY

CHRIS VU

CERTIFIED BY



IMPORTANT

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PKAAAIK

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CERTIFICATE OF ANALYSIS / EPA PROTOCOL GAS

CUSTOMER

HORIZON AIR MEASUREMENT

P.O NUMBER

REFERENCE STANDARD

COMPONENT

1.

NIST SRM NO.

CYLINDER NO.

CONCENTRATION

CARBON MONOXIDE GMIS

vs.SRM#1679

CC 43032

99.1 ppm

GMTS NITRIC OXIDE

vsSRM1684b

SA 21535

100.3 ppm

ANALYZER READINGS

R=REFERENCE STANDARD

Z=ZERO GAS

C=GAS CANDIDATE

i.	COMPONENT CARBON MONOXI	DE GMIS ANALYZ	ER MAKE-MODEL-S/N	Siemens Ultramat 5E S/N Al2-	729
	ANALYTICAL PRINCIPLE	NDIR		LAST CALIBRATION DATE	01/09/03
	FIRST ANALYSIS DATE	01/15/03		SECOND ANALYSIS DATE	01/21/03
	Z 0.0 R 99.1	C 79.3 CONC.	79.3 Z 0.0	R 99.1 C 79.2	CONC. 79.2
	R 99.1 Z 0.0	C 79.3 CONC.	79.3 R 99.1	Z 0.0 C 79.2	CONC. 79.2
	Z 0.0 C 79.3	R 99.1 CONC.	79.3 Z 0.0	C 79.2 R 99.1	CONC. 79.2
	U/M ppm	MEAN TEST ASSAY	79.3 ppm U/M ppm	m MEAN TES	T ASSAY 79.2 ppm
2.	COMPONENT NITRIC OXIDE	GMIS ANALYZ	ER MAKE-MODEL-S/N	Beckman 951A S/N 0101354	
	ANALYTICAL PRINCIPLE	Chemiluminescence		LAST CALIBRATION DATE	01/08/03
	FIRST ANALYSIS DATE	01/15/03		SECOND ANALYSIS DATE	01/21/03
	Z 0.0 R 887.5	C 707.1 CONC.	79.9 Z 0.0	R 888.7 C 709.1	CONC. 80.0
	R 888.5 Z 0.0	C 708.5 CONC.	80.0 R 890.9	Z 0.0 C 708.6	CONC. 79.7
	Z 0.0 C 709.6	R 889.8 CONC.	80.0 Z 0.0	C 708.1 R 888.1	CONC. 80.0
	U/M mv	MEAN TEST ASSAY	80.0 ppm U/M mv	MEAN TES	ST ASSAY 79.9 ppm

Values not valid below 150 psig. NOx values for reference use only.

THIS CYLINDER NO.

CC 157902

CERTIFIED CONCENTRATION

HAS BEEN CERTIFIED ACCORDING TO SECTION OF TRACEABILITY PROTOCOL NO.

Rev. 9/97

CARBON MONOXIDE EPA-600/R97/121

79.2 ppm

NITRIC OXIDE

NITROGEN

80.0 ppm

PROCEDURE CERTIFIED ACCURACY ± 1

% NIST TRACEABLE

BALANCE

CYLINDER PRESSURE

NOx

80.0 ppm

CERTIFICATION DATE

2000 PSIG

01/21/03

EXPIRATION DATE

01/21/05

TERM 24 MONTHS

ANALYZED BY

CERTIFIED BY

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CERTIFICATE OF ANALYSIS

CUSTOMER

HORIZON AIR MEASUREMENTS

DATE

03/31/03

P.O NUMBER

8156

REF. NUMBER

89360800

REQUESTED COMPOSITION

GAS

CONCENTRATION

CARBON DIOXIDE

OXYGEN

NITROGEN

BALANCE

ANALYTICAL ACCURACY

± 1 %

ANALYTICAL METHOD

INSTRUMENT

ANALYTICAL PRINCIPLE

METTLER ID5, S/N:1865166

GRAVIMETRIC

METTLER IDS, S/N:1865166

GRAVIMETRIC

VALUES NOT VALID BELOW 150 PSIG.

THIS CYLINDER NO.

CC 163394

CERTIFIED CONCENTRATION

CYLINDER PRESSURE

2000 PSIG

CARBON DIOXIDE

7.00%

EXPIRATION DATE

03/28/06

OXYGEN

12.01%

CLASSIFICATION

PRIMARY STANDARD

NITROGEN

BALANCE

BATCH NUMBER

LOT NUMBER

ANALYTICAL ACCURACY

PART NUMBER

109308406

CYLINDER SIZE AS CGA

EV NICDOXP1-AS

148 CFT

ANALYZED BY

CERTIFIED BY

PHU TIEN NGUYEN

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CERTIFICATE OF ANALYSIS

CUSTOMER

HORIZON AIR

DATE

08/27/02

P.O NUMBER

REF. NUMBER

00874800

REQUESTED COMPOSITION

GAS

CONCENTRATION

CARBON DIOXIDE

12 %

NITROGEN

BALANCE

ANALYTICAL ACCURACY il %

ANALYTICAL METHOD

INSTRUMENT

METTLER ID5, S/N:1865166

ANALYTICAL PRINCIPLE

GRAVIMETRIC

VALUE NOT VALID BELOW 150 PSIG.

THIS CYLINDER NO.

SA 2515

CERTIFIED CONCENTRATION

12.01 %

CYLINDER PRESSURE **EXPIRATION DATE**

2000 PSIG

CARBON DIOXIDE

CLASSIFICATION

08/27/05 PRIMARY STANDARD

NITROGEN

BALANCE

BATCH NUMBER

ANALYTICAL ACCURACY ±1 %

LOT NUMBER

N/A

CYLINDER SIZE AS CGA 580

109223508

PART NUMBER

EV NICD12P-AS

143 CFT

ANALYZED BY

CERTIFIED BY

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Magnehelic Gauge Calibration Data

Range:

0.0-1.0

Date:

02/17/03

Calibrated by:

Travis Williams

BAROMETRIC PRESURE:

29.40

Reference:

0.0-10.0" MANOMETER

SYSTEM

LEAK CHECKS (Y/N):

Y

POINT

LEAK CHECK (Y/N):

Υ

Magnahelic Box #

Serial #

R970865M62

MAG	MAN R1	MAN R2	MAN R3	MEAN	MEAN/MAG
0.20	0.20	0.20	0.20	0.200	0.998
0.40	0.40	0.40	0.40	0.400	0.999
0.60	0.60	0.60	0.60	0.599	0.999
0.80	0.80	0.80	0.80	0.800	1.000
1.00	1.00	1.00	1.00	1.000	1.000
			-		

Correction Factor:

0.9992

Date: 02.17.03

Checked by:

STACK TEMPERATURE SENSOR CALIBRATION DATA- APEX PROBE ASSEMBLIES

Date: 01/30/03 Calibrated by:

Travis Williams

THERMOCOUPLE

	ICE WATER								BSOLU DIFF.,			BOIL	ING WA	TER				BSOLU DIFF.,			P.	DILLING 0	41				SOLUT	
	_	REF				TC			·			REF	-	_	TC	_					REF				_		DIFF.,	×.
	1	2	3		1	2	3	1	2	3	1	2	3	1	2	3	1	2	3	1		_		TC				
64-t-t-			_		-						_		_	_					<u> </u>	<u>'</u>	2	_ 3	1	2	_a _	1	2	3
	ss Steel Pi	robes																										
4-2	32	32	3	32	32	32	31	0,0	0.0	0.2	212	212	212	212	212	213	0.0	0,0	-0.1	539	539	538	540	540	539	-0.1	-0.1	
4-3	32	32	3	32	32	32	33	0.0	0.0	-0.2	212	211	211	211	211	211	0.1	0.0	0.0	369	369	369	389	369	369			-0.1
6-2	32	32	3	32	33	33	32	-0,2	-0.2	0,0	211	212	212	212	212	212	-0.1	0.0	0.0	370	370	370		•			0.0	0.0
6-3	32	32	3	32	33	32	32	-0.2	0.0	0.0	212	212	212	213	213	213	-0.1	-0.1	-0.1	538			370	369	370	0,0	0.1	0.0
6-4	32	32	3	5	32	32	32	0.0	0.0	0.0	211	212	212	211	212	212	0.2	0.0			536	538	536	536	537	0,0	0.0	-0.1
A8-5	32	32	3	12	32	33	33	0.0	-0.2	-0.2	212	212	212	212	212	213			0.0	369	369	369	369	369	370	0.0	0.0	-0.1
A8-1	32	32	3	2	33	33	32	-0.2	-0.2	Ó.O	212	212	212	213			0.0	0.0	-0.1	535	535	535	534	535	535	0.1	0,0	0.0
A8-2	32	32	3:	2	23	33	32	-0.2	-0.2	0.0	212				218	213	-0.1	-0.1	-0.1	540	540	540	540	540	540	0.0	0.0	0.0
10-1	32	32	3:		32	32	32	0.0	0.0			212	212	212	212	213	0.0	0,0	-0.1	541	542	542	541	542	541	0,0	0.0	0.1
Inconel		_	_	-	 .	OL.	O.	0.0	0.0	0,0	212	212	212	212	212	212	0,0	0,0	0.0	540	539	529	540	540	539	0.0	-0.1	0.0
10-2 Inc	32	32	32		~~	~~																						
6-1 inc	32				a a	33	33	-0.2	-0.2	-0.2	212	212	212	213	213	213	-0.1	-0.1	-0.1	542	542	542	541	541	542	0.1	0.1	0.0
		. 32	32	2	33	33	32	-0.2	-0.2	0.0	212	212	212	213	213	213	-0.1	-0.1	-0.1	541	541	540	541	541	540	0.0	0,0	0.0
	hermocoup	de																										
6-5 <u>L</u>	32	32	32	2	33	32	32	-0.2	0.0	0.0	212	212	212	212	212	213	0,0	0.0	-0.1	540	540	540	539	540	541	0.1	0.0	-0.1
7-1L	32	32	32	2	32	31	32	0.0	0.2	0.0	212	212	212	212	213	213	0.0	-0.1	-0.1	540	540	540	539	539	539	0.1	0.1	
M17-1	32	32	32	?	33	33	32	-0.2	-0.2	0.0	212	212	212	211	212	212	0.1	0.0	0.0	370	270	369	369	369				0.1
3-1	32	32	32	;	32	32	32	0.0	0.0	0.0	212	212	212	212	213	212	0.0	-0.1	0.0	540	540	540			369	0.1	0.1	0,0
5-1	32	32	32	!	32	32	32	0.0	0.0	0.0	212	212	212	213	213	212	-0.1	-0.1	0,0	540			539	540	540	0.1	0,0	0.0
7-2	32	32	32	!	31	31	32	0.2	0.2	0.0	212	212	212	211	211	211	0.1	0.1			540	540	540	540	541	0.0	0,0	-0.1
																	V.1	V. 1	0.1	524	524	525	525	525	526	-0.1	-0,1	-0.1
6-7 6-8	32 32	32 32	32 32		32 32	32 32	32 31	0,0 0.0	0,0 0.0	0.0 0.2	212 212	212 212	212	212	212	212	0.0	0.0	0.0	535	535	535	535	534	535	0.0	0.1	0.0
8-3 Note: If	32	32	32		32	32	31	0.0	00	A 2	245	~4~	212 212	212 211	212 211	213 212	0,0 0,1	0.0 0.1	-0.1 0.0	521 514	521 514	521	520	520	521	0,1	0.1	0.0
·*************************************	absolute t no correcti	on is no	sere vi seded.		or the	e Lajet	ence t	hermon	ieter b	eing celli	brased an	d the sta	ck temp	، فلارتداد	ensone	ngree w	Athin 1.	5 perc	ent at oc	ch of the t	hree cal	ibration	points,	514	513	0,0	0,0	0.1

OT Whether

Control Box Calibration Data

Date:

01/29/03

Calibrated by:

FJOTorres

Meter Box Number:

4

Barometric Pressure:

29.31

Wet Test Meter Cf:

1.0013

	Gas	Volumes		Те	mperatu	res	Time	Y	H@
Orifice setting (H)	Wet Test (cu.ft)	Dry Gas Initial (cu.ft)	Dry Gas Final (cu.ft)	DGM Initial (°F)	DGM final (°F)	WTM (°F)	(min)		
0.5	6.200	719.365	725.627	69	70	71	15	0.9873	1.6812
1.0	5.788	737.182	743.028	70	71	71	10	0.9870	1.7131
1.5	10.335	725.907	736.320	69	71	71	15	0.9877	1.8142
2.0	18.346	680.992	699.487	71	73	71	23	0.9892	1.7989
3.0	14.536	666.152	680.763	69	73	71	15	0.9883	1.8307
4.0	19.350	646.527	665.885	65	72	71	17	0.9858	1.7777
							-		<u></u>
					,	AVERA	SE.	0.9876	1.7693

Reviewed by: Wacher

Control Box Calibration Data

Date:

02/05/03

Calibrated by:

FJOTorres

Meter Box Number:

5

auflactut

Barometric Pressure:

29.30

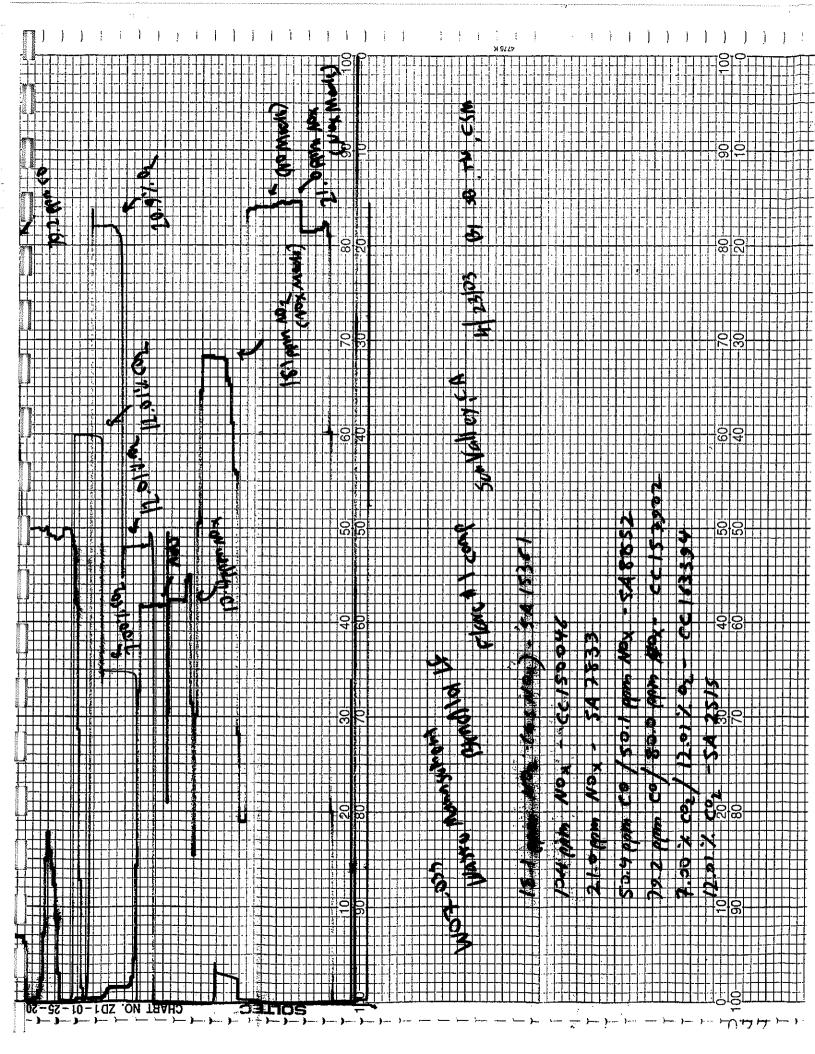
Wet Test Meter Cf:

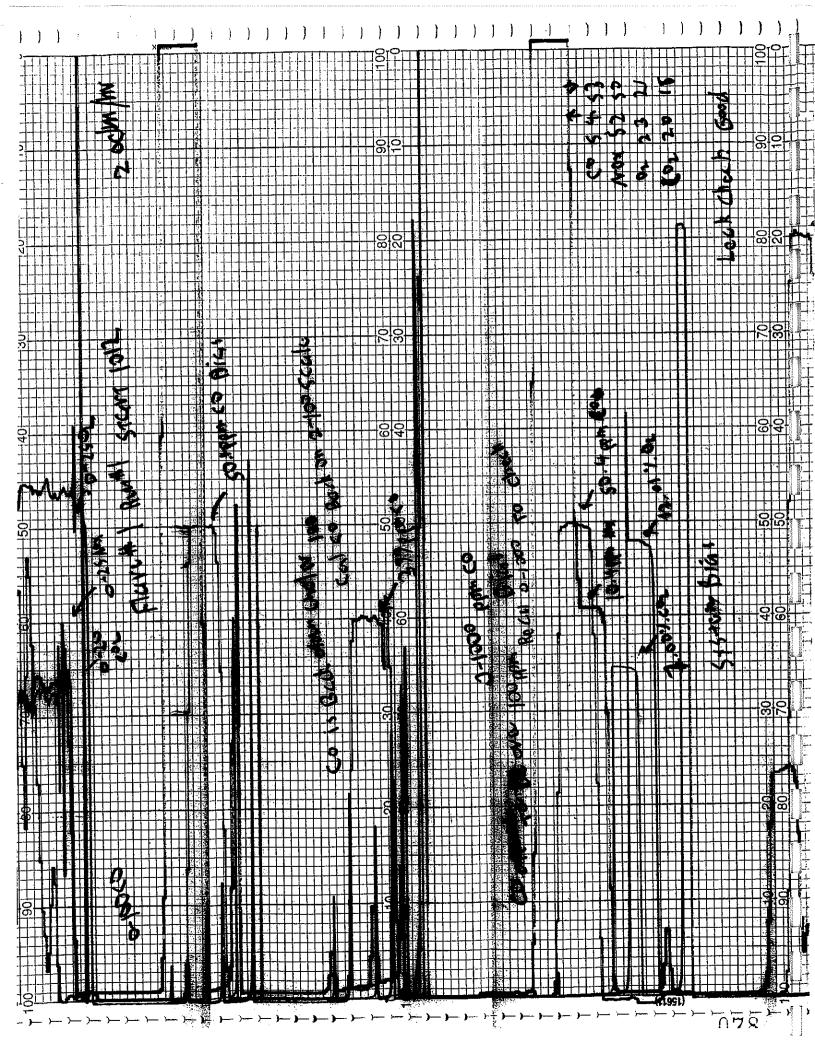
1.0013

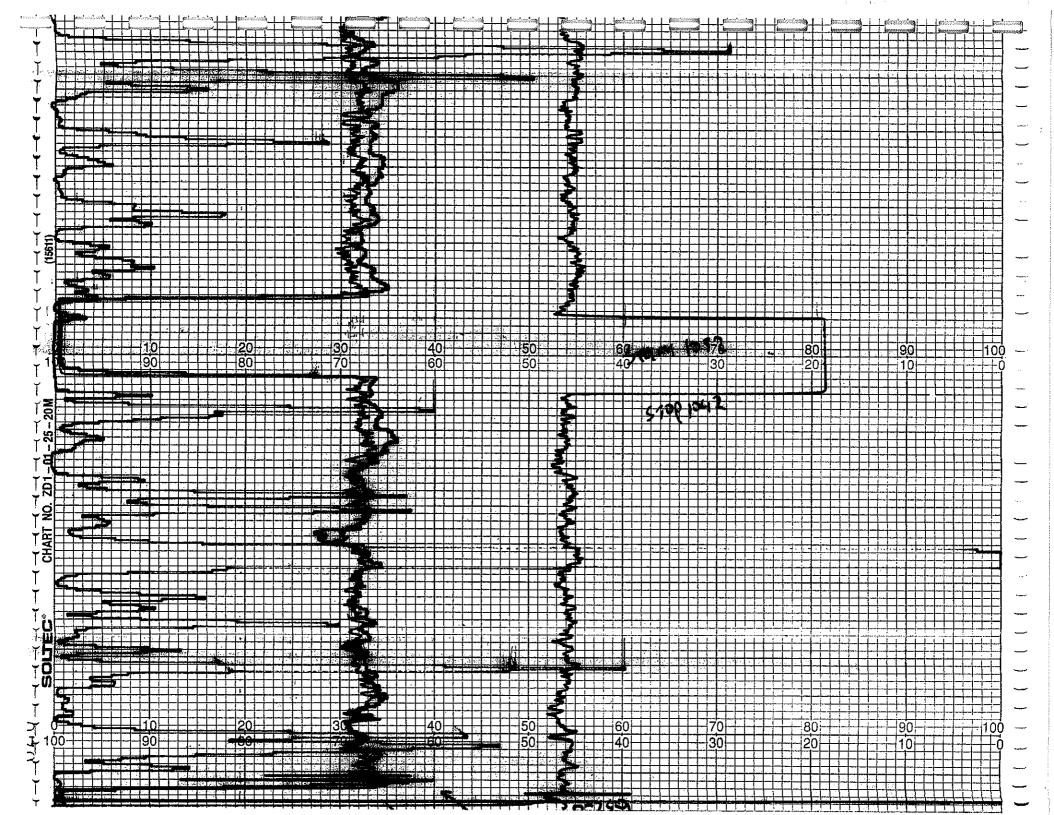
Gas Volumes			Temperatures			Time	Y	H@	
Orifice setting (H)	Wet Test (cu.ft)	Dry Gas Initial (cu.ft)	Dry Gas Final (cu.ft)	DGM Initial (°F)	DGM final (°F)	WTM (°F)	(min)		
0.5	7.054	436.875	444.083	67	76	65	17	0.9903	1.6258
1.0	19.763	504.138	524.342	69	77	66	34	0.9891	1.6595
1.5	13.236	524.559	538.157	77	80	67	19	0.9913	1.7218
2.0	16.216	474.603	491.257	73	79	66	20	0.9876	1.6962
3.0	11.951	461.997	474.270	71	78	66	12	0.9829	1.6903
4.0	16.120	445.166	461.642	69	77	66	14	0.9824	1.6908
							_		
						AVERAC	SE .	0.9873	1.6807

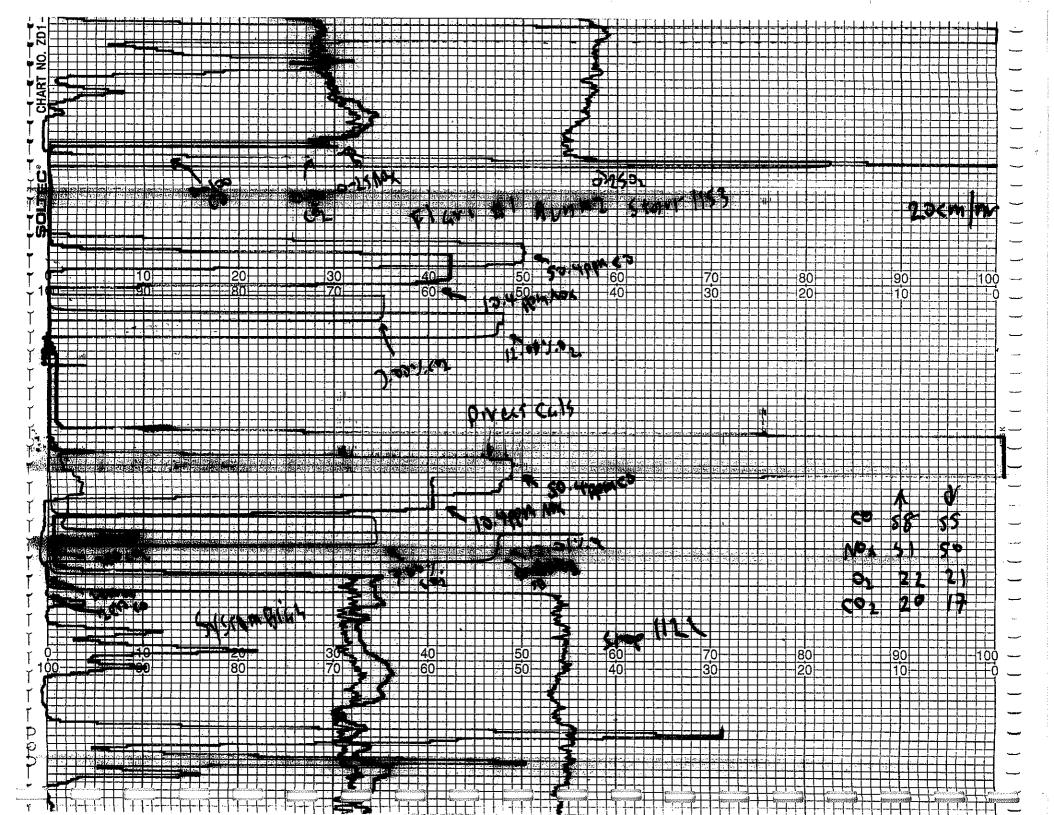
Reviewed by:

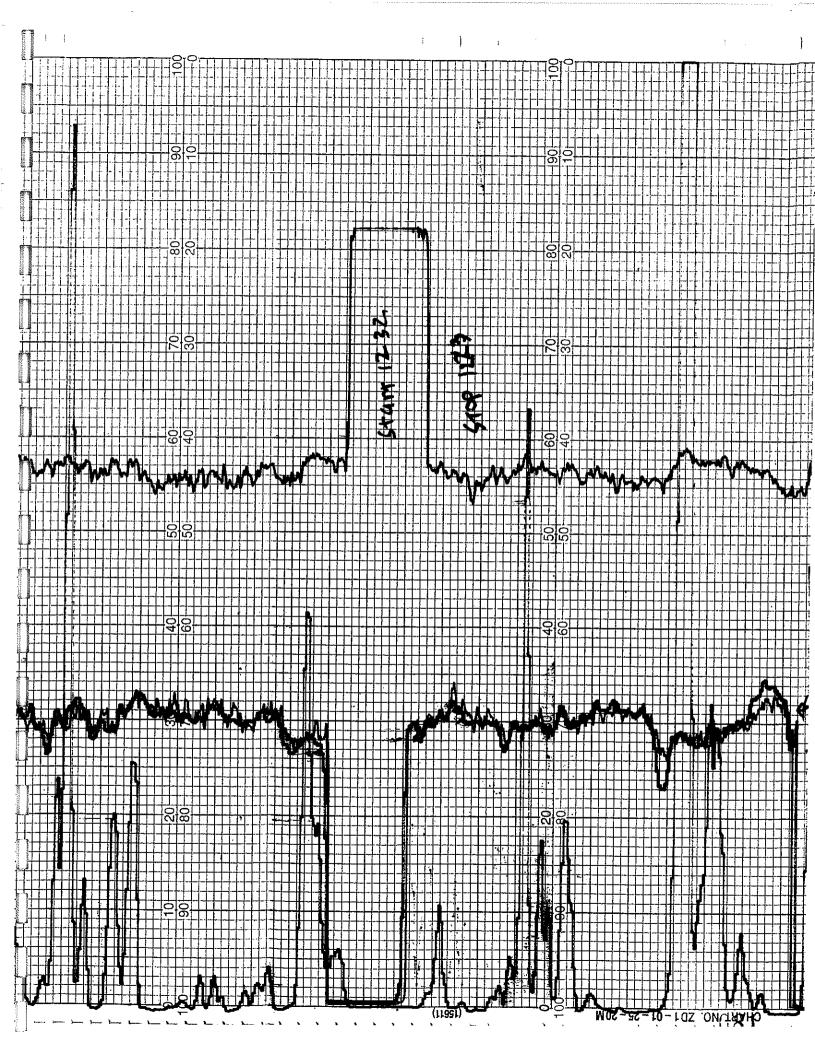
APPENDIX F - Strip Chart Data

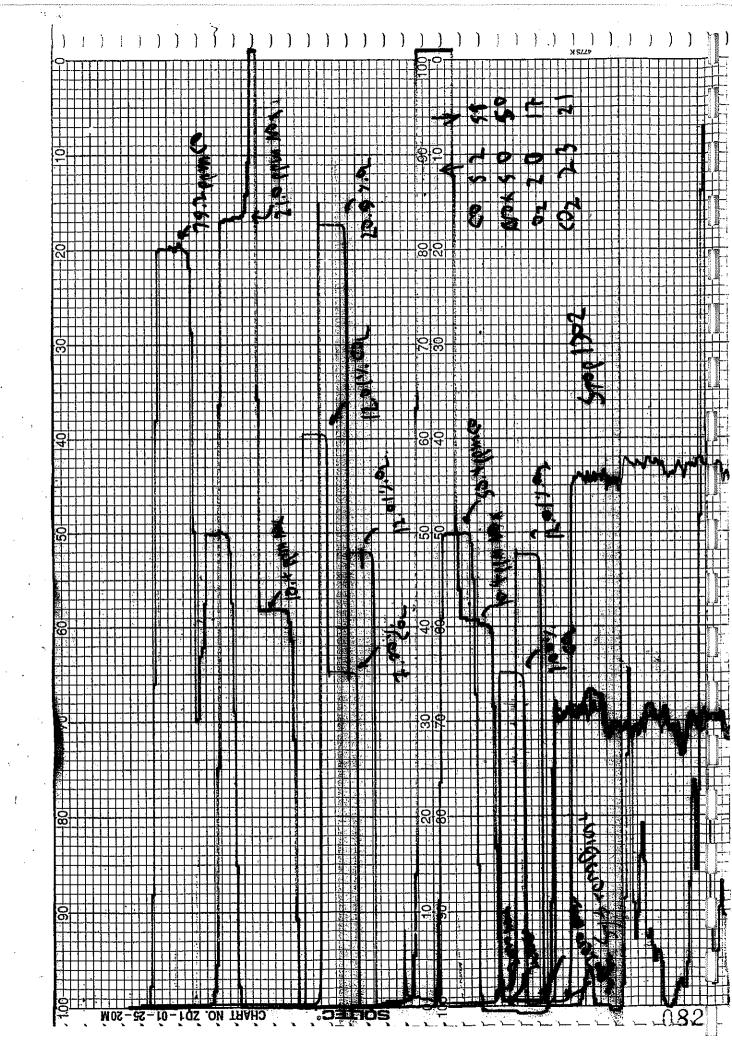












APPENDIX G - Process Data

OPERATING DATA FOR LANDFILL FLARES

Facility: Bradley Land Fill Date: 4/23/03Job No.: 1/2Source: 1/2

Time Run#1	Landfill Gas Flow (SCFM)	Condensate Injection (G-PM)	Flare Temerature (°F)	Fuel Pressure	Fuel Temp (°F)	
1015	3567	3.5	1656	NA	NA	
1025	3605	3.5	1640			
1035	3611	3.5	1652			
1045	3591	3,5	1649			
1055	3624	3.5	1650			
1105	3658	3.5	1619			
Run#2		_			,	
1200	3642	3.5	1646			
1210	3640	3.5	1621			
1220	36 27	3.5	1630			
1230	3618	3.5	1834		,	
1240	3642	3.5	1054			
1250	3635	3.5	1629		•	
				ų .		

3,621 3.5 1,640

APPENDIX H - Permit to Operate



PERMIT TO CONSTRUCT

Application No.

DECEIVED

9/22/60

Granted as of 9/12/2000

LEGAL OWNER OR OPERATOR:

BRADLEY LANDFILL AND RECYCLING CENTER
9081 TUJUNGA AVE P O BOX 39

SUN VALLEY, CA. 91352

ID 050310

Equipment Location:

9227 TUJUNGA AVE, SUN VALLEY, CA 91352-1542

Equipment Description:

LANDFILL GAS FLARING SYSTEM NO. 1 CONSISTING OF:

- 1. LIQUID KNOCKOUT/PARTICULATE REMOVAL VESSEL, JOHN ZINK, 2'-6" DIA. X 6'-0" H.
- 2. TWO BLOWERS, ONE STANDBY, LANDFILL GAS, EACH 200 HP, EACH 5,556 SCFM MAXIMUM FLOW RATE.
- 3. FLARE NO. 1, JOHN ZINK, 13'-0" DIA. X 60'-0" H., WITH A MULTI-JET BURNER, A PROPANE GAS PILOT, ELECTRIC IGNITER, UV FLAME SENSOR, THERMOCOUPLE WITH TEMPERATURE INDICATOR AND RECORDER, AUTOMATIC SHUTDOWN AND ALARM SYSTEM, AUTOMATIC COMBUSTION AIR REGULATING SYSTEM, TEMPERATURE CONTROLLER AND FLAME ARRESTOR.

Conditions:

- 1) OPERATION OF THIS EQUIPMENT SHALL BE CONDUCTED IN ACCORDANCE WITH ALL DATA AND SPECIFICATIONS SUBMITTED WITH THE APPLICATION UNDER WHICH THIS PERMIT IS ISSUED UNLESS OTHERWISE NOTED BELOW.
- 2) THIS EQUIPMENT SHALL BE PROPERLY MAINTAINED AND KEPT IN GOOD OPERATING CONDITION AT ALL TIMES.
- 3) THIS EQUIPMENT SHALL BE OPERATED AND MAINTAINED BY PERSONNEL PROPERLY TRAINED IN ITS OPERATION.



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- THE START-UP FOR THIS FLARE SHALL NOT EXCEED 30 MINUTES. ANY OUTAGE THAT RESULTS IN THE SHUTDOWN OF THE FLARE OR GAS COMPRESSOR AND THE SUBSEQUENT START-UP OR RESTART OF THE FLARE OR THE COMPRESSOR IS NOT CONSIDERED A BREAKDOWN, PROVIDING NO RAW LANDFILL GAS EMISSIONS OCCUR.
- 5) THE FLARE SHALL BE EQUIPPED WITH A TEMPERATURE INDICATOR AND RECORDER WHICH MEASURES AND RECORDS THE GAS TEMPERATURE (IN DEGREES F) IN THE FLARE STACK. THE TEMPERATURE INDICATOR AND RECORDER SHALL OPERATE WHENEVER THE FLARE IS IN OPERATION.
- WHENEVER THE FLARE IS IN OPERATION, A TEMPERATURE OF NOT LESS THAN 1500 DEGREES F, AS MEASURED BY THE TEMPERATURE INDICATOR SHALL BE MAINTAINED IN THE FLARE STACK EXCEPT DURING START-UP TIME FOR NOT MORE THAN 30 MINUTES. THE THERMOCOUPLE USED TO MEASURE THE TEMPERATURE SHALL BE ABOVE THE FLAME ZONE AND AT LEAST 3 FEET BELOW THE TOP OF THE FLARE SHROUD AND AT LEAST 0.6 SECONDS DOWNSTREAM OF THE BURNER.
- 7) THE FLARE SHALL BE EQUIPPED WITH A FAILURE ALARM WITH AN AUTOMATIC BLOWER AND LANDFILL GAS SUPPLY VALVE SHUT-OFF SYSTEM APPROVED BY THE AQMD, IN ORDER TO ISOLATE THE FLARE FROM THE LANDFILL GAS SUPPLY LINE, TO SHUT-OFF THE BLOWER AND TO NOTIFY A RESPONSIBLE PARTY OF THE FAILURE.
- 8) THE SHUT-OFF SAFETY SYSTEM SHALL BE TESTED ANNUALLY FOR PROPER OPERATION AND THE RESULTS RECORDED.
- 9) A FLOW INDICATING AND RECORDING DEVICE SHALL BE INSTALLED IN THE LANDFILL GAS SUPPLY LINE TO THE FLARE TO MEASURE AND RECORD THE QUANTITY OF LANDFILL GAS (IN SCFM) BEING BURNED.
- 10) ALL RECORDING DEVICES SHALL BE SYNCHRONIZED WITH RESPECT TO THE TIME OF DAY.
- 11) A PRESSURE DIFFERENTIAL INDICATOR SHALL BE MAINTAINED ACROSS THE FLAME ARRESTOR.
- 12) CONDENSATE INJECTED INTO THE FLARE SHALL NOT EXCEED 5 GPM.
- 13) THE TOTAL VOLUME OF LANDFILL GAS BURNED IN THE FLARE SHALL NOT EXCEED 5,556 STANDARD CUBIC FEET PER MINUTE.
- 14) EMISSIONS RESULTING FROM THE FLARE SHALL NOT EXCEED THE FOLLOWING:
 POLLUTANT LBS/HOUR

ROG	1.86
NOX (AS NO2)	10.0
SOX (AS SO2)	8.44
co	33.3
PM10	3.0

- 15) EMISSIONS OF NOX FROM THE FLARE SHALL NOT EXCEED 0.06 LBS PER MILLION BTU OF HEAT.
- A SUFFICIENT NUMBER OF, SIGHT GLASS WINDOWS SHALL BE INSTALLED IN THE FLARE TO ALLOW VISUAL INSPECTION OF THE FLAME AND THERMOCOUPLE LOCATION WITHIN THE FLARE AT ALL TIMES. ADEQUATE AND SAFE ACCESS SHALL BE PROVIDED FOR ALL PORTS UPON REQUEST BY AQMD PERSONNEL.
- A SET OF FOUR SAMPLING PORTS SHALL BE INSTALLED IN THE FLARE SHROUD AND LOCATED AT LEAST TWO FEET ABOVE THE FLAME ZONE AND AT LEAST THREE FEET BELOW THE TOP OF THE FLARE SHROUD. EACH PORT SHALL BE INSTALLED AT 90 DEGREES APART AND SHALL CONSIST OF FOUR INCH COUPLINGS. ADEQUATE AND SAFE ACCESS TO ALL TEST PORTS SHALL BE PROVIDED BY THE APPLICANT WITHIN 24 HOURS OF A REQUEST BY THE AQMD TO CONDUCT A TEST.
- 18) A SAMPLING PORT, OR OTHER METHOD APPROVED BY THE AQMD, SHALL BE INSTALLED AT THE INLET GAS LINE TO THE FLARE.
- 19) THE SKIN TEMPERATURE OF THE FLARE SHROUD WITHIN FOUR FEET OF ALL THE SOURCE TEST PORTS SHALL NOT EXCEED 250 DEGREES F. IF A HEAT SHIELD IS REQUIRED TO MEET THIS REQUIREMENT, ITS DESIGN SHALL BE APPROVED BY THE AQMD PRIOR TO CONSTRUCTION. THE HEAT SHIELD, IF REQUIRED TO MEET THE TEMPERATURE REQUIREMENT, SHALL BE IN PLACE WHENEVER A SOURCE TEST IS CONDUCTED BY THE AQMD.
- 20) THE APPLICANT SHALL CONDUCT A SOURCE TEST ANNUALLY OR PER THE APPROVED 1150.1 COMPLIANCE PLAN. THE TEST SHALL BE PERFORMED IN ACCORDANCE WITH AQMD APPROVED TEST PROCEDURES. THE TEST SHALL INCLUDE, BUT MAY NOT BE LIMITED TO, A TEST OF THE FLARE FOR:
 - A. LANDFILL GAS COMPOSITION AND HEATING VALUE (INLET)
 - B. LANDFILL GAS FLOW RATE, SCFM (INLET)
 - C. TOTAL SULFUR COMPOUNDS AS H2S, PPMV (INLET)
 - D. TEMPERATURE, F (EXHAUST)
 - E. FLOW RATE, DSCFM (EXHAUST)
 - F. NOX, LBS/HR AND LBS/MMBTU (EXHAUST)
 - G. SOX, LBS/HR (EXHAUST)
 - H. CO, LBS.HR (EXHAUST)
 - I. PM, LBS/HR AND GR/DSCF (EXHAUST)
 - J. TOTAL NON-METHANE ORGANICS, LBS/HR (INLET AND EXHAUST)
 - K. RULE 1150.1 TOXIC COMPOUNDS, PPMV (INLET AND EXHAUST)

THE SOURCE TEST SHALL BE CONDUCTED AT THE MAXIMUM FLOW RATE AVAILABLE AT THE TIME OF THE TEST BUT NOT TO EXCEED THE FLOW RATE ALLOWED BY THIS PERMIT.

ANY BREAKDOWN OR MALFUNCTION OF THE LANDFILL GAS FLARE RESULTING IN THE EMISSION OF RAW LANDFILL GAS SHALL BE REPORTED TO THE AQMD WITHIN ONE HOUR AFTER OCCURRENCE, AND IMMEDIATE REMEDIAL MEASURES SHALL BE UNDERTAKEN TO CORRECT THE PROBLEM AND PREVENT FURTHER EMISSIONS INTO THE ATMOSPHERE.

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22) ALL RECORDS SHALL BE KEPT FOR A PERIOD OF AT LEAST TWO YEARS AND SHALL BE MADE AVAILABLE TO AQMD PERSONNEL UPON REQUEST. A RECORD OF THE HOURS OF FLARE OPERATION SHALL BE INCLUDED.

Approval or denial of this application for permit to operate the above equipment will be made after an inspection to determine if the equipment has been constructed in accordance with the approved plans and specifications and if the equipment can be operated in compliance with all Rules of the South Coast Air Quality Management District.

Please notify TED KOWALCZYK at (909) 396-2592 when construction of equipment is complete.

This Permit to Construct is based on the plans, specifications, and data submitted as it pertains to the release of air contaminants and control measures to reduce air contaminants. No approval or opinion concerning safety and other factors in design, construction or operation of the equipment is expressed or implied.

This Permit to Construct shall serve as a temporary Permit to Operate provided the Executive Officer is given prior notice of such intent to operate.

This Permit to Construct will become invalid if the Permit to Operate is defined or if the application is cancelled. THIS PERMIT TO CONSTRUCT SHALL EXPIRE ONE YEAR FROM THE DATE OF ISSUANCE unless an extension is granted by the Executive Officer.

DORRIS M. BAILEY
Principal Office Assistant

DMB/k01

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